U. S. ATOMIC ENERGY COMMISSION RAW MATERIALS DEVELOPMENT LABORATORY WINCHESTER, MASSACHUSETTS

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OPERATED BY

NATIONAL LEAD COMPANY, INC

Contract AT(49-6)-924

SUMMARY REPORT 1954 - 1959

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TOPICAL REPORT WIN-115

SUMMARY REPORT, 1954-1959

RAW MATERIALS DEVELOPMENT LABORATORY

WINCHESTER, MASSACHUSETTS

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GRAND JUNCTION, COLORADO

September 30, 1959

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Edited by R. G. Beyerly, Mgr. Grand Jct. Field Office Grand Junction, Colorado

Approved By:

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U. S. Atomic Energy Commission Contract No. AT(49-6)-924

NATIONAL LEAD COMPANY, INC. Raw Materials Development Laboratory Winchester, Massachusetts

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TABLE OF CONTENTS

	Page
INTRODUCTION	3
ACKNOWLEDGEMENTS	4
HISTORY OF THE PROJECT	5
RESUME OF RESEARCH WORK	7
Fundamental Research Applied Research Analytical Amenability Testing Pilot Plant Mill Assistance	7 7 10 10 11 14
DESCRIPTION OF FACILITIES	15
Winchester Laboratory Grand Junction Pilot Plant	15 15
PERSONNEL	25
PUBLICATIONS	28
PATENTS	30
APPENDIX	
Topical Reports classified by subject Contents of Monthly Progress Reports Uranium Ores tested and references WIN Reports and abstracts ACCO Reports and abstracts MITG Reports and abstracts	32 33 34 35 69 75

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INTRODUCTION

The recovery of uranium from its ores has been the subject of extensive research in several laboratories, under the sponsorship of the Raw Materials Division of the Atomic Energy Commission, for the last 15 years. A major role in this work has been played by the Raw Materials Development Laboratory, Winchester, Massachusetts, and the Raw Materials Development Pilot Plant, Grand Junction, Colorado. Since July 1954, these projects were operated for the Government by the National Lead Company. The purpose of this report is to review briefly the activities of the National Lead Company during the performance of this work and to present a guide to the uranium industry to aid in the location of research information pertinent to the winning of uranium from its ores.

Because much of the early work on this project, accomplished under the direction of M.I.T. and American Cyanamid Company, was reported at a time when raw materials technology was classified, a complete list of publications made by these two groups from 1944 to 1954 is presented in the appendix.

ACKNOWLEDGEMENTS

The National Lead Company would like to express its appreciation for the assistance and cooperation extended by Mr. E. C. Van Blarcom, Dr. G. G. Marvin, and Mr. J. C. Johnson, U.S. A.E.C., Washington, D. C. Their assistance was at all times helpful in the development of a full and successful raw materials development program. Thanks is also due Mr. A. E. Jones, U.S. A.E.C., Grand Junction, Colorado, and Mr. S. P. Wimpfen formally of that organization for their advice and encouragement on this program.

Mr. G. W. Wunder, Vice President and General Manager of the National Lead Company, Inc., contract operators for the Winchester Laboratory and the Grand Junction Pilot Plant, and Dr. Alex Stewart, retired, Vice President and General Manager, National Lead Company, Inc., contributed in considerable measure to the success of this project.

No attempt will be made here to credit the other research facilities engaged in uranium raw materials research for their individual contribution to the industry and to the program at the Raw Materials Development Laboratory. The excellent liaison and unselfish cooperation of the other research facilities in this work was of great value to the program.

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HISTORY OF THE PROJECT

The Raw Materials Development Laboratory had its beginning at the Massachusetts Institute of Technology under the direction of Professor A. M. Gaudin in July of 1944. At this time Lt. Col. J. E. Vance and Major P. H. Merritt of the Manhattan Engineering District conferred with M.I.T. personnel on the treatment of Congo rejects for the extraction of uranium. The initial purpose of the project was to study the treatment of low-grade uranium ores with emphasis on the principles involved rather than for the specific solution of any one problem. The initial plan was modest.

As the work developed, it became clear that ore of much lower grade would have to be treated to provide increased uranium production. The project, therefore, was increasingly orientated to the effective processing of relatively low-grade materials. As the problems increased in variety and complexity, as well as in significance, the site of the research facilities was moved to larger quarters at the Watertown Arsenal, Watertown, Massachusetts. The project remained under the direction of the M.I.T., Mineral Engineering Laboratory, at Watertown until March 1951. During the seven years that this group worked on the problems of winning uranium from its ores, tremendous progress was achieved in the hydrometallurgy of uranium. Much credit is due Professor Gaudin and his organization for the successful start of the Raw Materials Development Laboratory. In March 1951 the management of the project was assumed by American Cyanamid Company under the direction of Mr. D. M. Kentro. American Cyanamid operated the project until July 1954. During this period the technology of processing uranium ores was greatly advanced not only by the group under American Cyanamid but other research institutions in the field such as Battelle Memorial Institute, Arthur D. Little, Inc., Columbia University, The Merrill Company, Dow Chemical Company, and others.

During this period the new quarters of the laboratory at Winchester, Massachusetts, were constructed. This laboratory is described in detail under the section of this report entitled, "Description of Facilities." During this period the first small pilot plant was constructed at Grand Junction for the express purpose of developing the resin-in-pulp process.

In July of 1954, the project was taken over by the National Lead Company, Inc. Dr. Alex Stewart, Director of Research for the National Lead Company, was Vice President and General Manager of National Lead Company, Inc., and Mr. J. S. Breitenstein was Technical Director of the project. Under National Lead Company, the large pilot plant was completed in Grand Junction and the project reached its peak of activity. During the period that the project has been in operation, the domestic uranium raw materials industry grew from a small-scale operation, dependent on a few small vanadium-uranium mills, to a large efficient industry, mining and processing many millions of tons of ore each year. The contribution of the research groups that developed the metallurgical processes that are in use in the uranium mills to the growth of the industry was enormous. Not only was the cost of processing the ore continuously reduced but low-grade and refractory deposits of ore were rendered amenable through technological advances.

RESUME OF RESEARCH WORK

Fundamental Research

In chemical processing, a fundamental knowledge of the chemical reactions involved is important since such an understanding usually discloses means of improving existing processes. Several investigations which may be classed as fundamental research, were conducted at the laboratory.

As the need arose fundamental research was conducted in connection with leaching, oxidation-reduction, ion exchange, solvent extraction, and precipitation. One such specialized piece of research work on which relatively more time was spent included a study of the kinetics and mechanism of the reactions involved in the dissolution of uranium in carbonate-bicarbonate solutions which established the order of magnitude of the variables. An interesting sidelight of this study was the development of a technique for using powdered specimens in the kinetic studies of liquid-solid systems.

Because of the importance of vanadium in alkaline leach - chemical precipitation circuits, the study of the nature of vanadium species in carbonate solutions and the interaction of vanadium and uranium in alkaline systems was carried out. Definite evidence of uraniumvanadium interaction was observed, thereby explaining the difficulty in selectively precipitating uranium from carbonate solutions of appreciable vanadium content.

In connection with the recovery of uranium from acid leach liquors a study was made to determine the structure of the uranyl sulfate complex ion species formed in the extraction of uranium with amine solvents.

Applied Research

In the ion exchange field, the laboratory actively engaged in a program of resin testing which included cooperation with resin manufacturers in checking new resin products to determine the adaptability of new resins or resin forms to uranium recovery processes. Another ion exchange project was devoted to the investigation of molybdenum poisoning. As a result of this investigation, an eluant was found which removes the molybdenum from the resin readily and inexpensively. Methods of molybdenum removal from leach liquor by charcoal adsorbtion and partial neutralization were also tested extensively.

Results of fundamental ion exchange studies indicated that an alkaline resin-in-pulp process was feasible. Simultaneous pilot

plant and laboratory programs developed this scheme into a practical and economic process. Studies on pH control showed effective methods of preferentially loading uranium and eliminating vanadium.

A continuous, countercurrent, resin-in-pulp flowsheet was developed and tested in the laboratory. Uranium was adsorbed in three or four stages compared to eight to ten stages required in conventional basket-type RIP systems and was subsequently removed from the resin by continuous countercurrent elution either in a column or tanks.

Uranium reduction processes employing sodium amalgam and hydrogen were studied in the laboratory as alternate methods for uranium precipitation from carbonate leach liquors to supplant the caustic precipitation method. The sodium amalgam process did not look attractive but the hydrogen reduction method offered more promise and was tested in the Pilot Plant. When laboratory and pilot plant tests indicated organic material in some ores interfered with leaching and uranium precipitation in alkaline circuits, a program was initiated to develop methods of minimizing this interference. Adsorption on charcoal and electrolytic oxidation of the organic material were two of the methods most actively pursued toward elimination of this problem.

Of particular importance to the uranium industry was the research conducted on improving uranium extractions during carbonate leaching. Following a study of chemical oxidants, it was found that the oxidation of uranium by air in the presence of copper-ammonia complex ions as a catalyst resulted in efficient dissolution of uranium at a cost considerably less than was possible with potassium permanganate.

Solvent extraction studies led to the development of the Eluex process by which sulfuric acid eluates from an RIP system are solvent extracted, the uranium is stripped from the solvent, and then precipitated from the high-grade, high-purity strip solution. Advantages of the process are lower reagent consumption, elimination of nitrate from the system, and a low-impurity, high-grade product.

Considerable laboratory work was done on a process consisting of direct solvent leaching of uranium from acid-pugged ores. Although a simple mechanical method for performing the operation was not found, attractive features were the recovery of uranium from essentially dry ore so that the solid-liquid separation step required after conventional leaching procedures might be eliminated. Results demonstrated the workability of the process but cost evaluations indicated that, at the time, the process was not competitive with more conventional milling processes.

Working closely with the manufactures, the laboratory evaluated a large number of new amine solvents, and this close cooperation accelerated the development of new uranium extractants which greatly increased the flexibility of the solvent extraction process while reducing chemical costs.

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One of the major efforts of the laboratory and pilot plant was the development of a process for recovery of uranium from uraniferous lignites. After extensive laboratory tests on roasting, leaching, and solvent extraction, a flowsheet was developed which was evaluated in the pilot plant. This work solved a particularly difficult extraction problem since these ores proved to be nonamenable to alkaline leaching and the acid leach and ion exchange approach was complicated by the presence of high concentrations of molybdenum, iron, sulfate, and organic matter in the leach solutions.

A new process for the production of green salt (UF_4) was developed which consists of preparation by solvent extraction of a highly purified and concentrated uranium solution and precipitation of dense UF_4 by catalytic reduction with sulfur dioxide. The process is unique in that the feed material may be an acid leach solution or any other solution from which uranium can be solvent extracted. The UF_4 product meets the exacting chemical and physical specifications required for the production of metal from the green salt. The chemical costs of the process are only slightly greater than the cost of producing yellow cake. The process steps are simple and the capital cost is not significantly greater than that of conventional solvent extraction circuits producing yellow cake.

The recovery of uranium from magnesium fluoride slag and bomb liner material originating at the uranium metal refineries was also intensively studied. A simplified sulfuric acid leaching and solvent extraction process was developed which will recover the uranium as a very high-grade yellow cake or a UF₄ product at low capital and operating costs.

The past year of research work at the laboratory has been devoted almost exclusively to finding and testing a method by which radioactive contaminants could be removed economically from uranium mill tailings. Radium and thorium are the primary radioactive contaminants in the mill waste streams and research was largely confined to measuring and studying means to reduce these materials. A process for treatment of acid mill tailings was resolved that involved neutralization of the tailings solution followed by barite treatment either in agitated tanks or in a percolation bed. For alkaline mill tailings a process involving decontamination by a two-stage flocculation and barite treatment was developed. Coagulation was accomplished by use of a commercial water treatment reagent such as ferrous sulfate. By such treatment acid and alkaline mill tailings can be decontaminated sufficiently to meet the specification established by the A.E.C. for waters released to unrestricted areas.

A list of general research subjects investigated and topical reports issued on each is shown in Appendix Table 1. Table 2 shows the general subjects covered in each of the monthly progress reports.

Analytical

As analytical methods were developed and as special analytical problems dealing with uranium and related assays were solved, the techniques were recorded and published in the "Raw Materials Development Laboratory Handbook of Analytical Methods." This manual, which was supplied to interested laboratories throughout the uranium industry and the A.E.C., is available as Technical Information Service Report TID-7002 (Rev. 1).

A great deal of effort was expended on devising an apparatus for the automatic, continual determination of uranium in ion exchange effluents and solvent extraction raffinates. The continuous assaying of ion exchange effluents was successfully demonstrated in the laboratory but extensive engineering would be required to make the apparatus more compact and rugged for use in a mill.

Improving the fluorometric method of uranium determination was a continuing program at the Winchester Laboratory. During 1957 and 1958 the method was improved when the fluorometer was converted to operate without a reference source and an automatic fusion burner was designed and installed. Assistance was provided in making these changes at various mills in this country.

Development of new assaying techniques or revisions of existing methods was necessary when the project program was diverted to radioactive pollution studies. The carrier-free method developed for the determination of radium utilizes a lead sulfate carrier precipitation and an ion exchange separation of lead from radium followed by counting an aliquot dried on a planchet. A similar carrier-free method was also developed for thorium.

A major part of the work of the Analytical Department consisted of routine analyses for the other laboratory departments and special assays for these as well as the Pilot Plant. For several years the number of these determinations averaged 5000 assays per month.

Amenability Testing

Amenability testing was largely confined to ore testing and new product evaluation. Approximately 375 ores from 62 different locations were studied in the laboratory. The ores were tested to determine optimum conditions for extracting the uranium by acid and alkaline leaching, to obtain information on the rate of filtration and settling, and to determine the characteristics of the pregnant leach solution with respect to recovery of uranium by chemical precipitation, ion exchange, or solvent extraction. Table 3 of the appendix shows the ores studied and references to where the information was reported.

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Product testing was conducted on a variety of products submitted by manufacturers for evaluation. Among such products were new resins and extractants, flocculating and dispersing agents for controlling the physical properties of ore pulps, activated carbon for adsorption of molybdenum and organic material, filter cloths and filter aids, and various miscellaneous chemicals.

<u>Pilot Plant</u>

The pilot plant program after 1954 was largely two-fold in purpose: (1) Amenability testing of uranium ores from a wide variety of commercial deposits to obtain metallurgical and cost data and (2)to develop and test new processes in pilot plants of sufficient size to permit accurate scale-up to commercial plants. The equipment available for testing ores permitted essentially any desired flowsheet which appeared most efficient for a particular ore from the results of laboratory amenability testing. During most of the project three pilot plants were in continuous operation, each with a capacity of 5 - 15 tons of ore per day. All pilot plants were operated on a 24-hour day, 7-day week basis.

A typical pilot plant amenability test consisted of a 6 weeks to 2 months operation during which time a 500 - 1000 ton representative sample of an ore body or mine was processed. The flowsheet used and operating conditions were largely predicated on earlier laboratory work and the more important variables were also studied in the Pilot Plant. In some cases where very extensive ore bodies indicated that several mills would be built, the ore was tested in two or more pilot plants to obtain complete metallurgical and cost data for comparing economics of various processes. Pilot plant data included over-all uranium recovery, metallurgical data such as optimum grind, leaching conditions and effects of oxidants, filtration or thickening rates, ion exchange data including possible poisoning materials, solvent loading, stripping, and disengagement data, ion exchange column studies, precipitation procedures, and product grade and impurities; as well as total reagent consumption figures for every condition tested. From this information it was possible to calculate reagent costs and to size equipment for commercial mills.

After development of the acid leach - resin-in-pulp process, 19 different ores were tested for their amenability to this method of treatment. As a result six mills were built which used the RIP process, located at Monticello and Moab, Utah; Grants, New Mexico; Tuba City, Arizona, Jeffrey City, Wyoming; and Edgemont, South Dakota. One mill has been built at Maybell, Colorado, using the countercurrent RIP system and two mills under construction in Wyoming are considering this technique of uranium recovery.

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The Eluex process, a modification of the elution and uranium recovery method connected with RIP was extensively tested in the Pilot Plant and has been put into operation at the Edgemont, South Dakota, mill.

Alkaline leaching of uranium ores in agitated open tanks and in Pachuca tanks, operating at both atmospheric pressure and at relatively small increases in pressure and temperature, was studied during the early part of the pilot plant program. During 1956 and 1957 considerable work was performed on alkaline pressure leaching. A few of the variables studied in the 1000-gallon autoclave included temperature, pressure, air addition, contact time, and agitation. These studies showed that all of these variables were interrelated and each must be considered in selecting optimum operating conditions.

As a follow-up to the work done at Winchester on oxidants for alkaline leaching the copper-ammonia oxidant was tested in the Pilot Plant. Following adoption of copper-ammonia at the Monticello uranium mill results showed that, compared to potassium permanganate, an estimated savings of three dollars per ton of ore treated was realized; one dollar per ton for lower reagent cost and two dollars per ton as a result of increased uranium recovery.

A circuit was installed to investigate continuous precipitation of uranium with caustic from pregnant alkaline liquors. Another method of precipitating alkaline liquors, by hydrogen reduction in the presence of nickel catalyst, was also tested.

Results of pilot plant work on some fourteen different types of ores in the alkaline leaching process were a contributing factor in the building of seven mills incorporating sodium carbonate bicarbonate dissolution processes. Four of these mills are located at Grants, New Mexico, with other mills at Monticello, Utah; Canon City, Colorado; and Riverton, Wyoming. Pressure leaching, copper-ammonia oxidation, and continuous precipitation techniques have all been employed in one or more of these mills.

The pilot testing of the alkaline leach - resin-in-pulp process lead to the conversion of the A.E.C. Monticello mill and to the change of a portion of the Uranium Reduction Company mill to this recovery method. Alkaline leaching followed by CCD for liquidsolid separation and column ion exchange was also tested and found to be technically possible. Acid leach - CCD - IX plants could be easily converted to the process should the need arise.

Another combined process tested in the Pilot Plant included_ flotation of the lime portion of high-lime ore followed by alkaline leaching of the high-lime fraction and acid leaching of the flotation tails, or low-lime fraction.

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Ores from the Big Indian Wash area of Utah, Ambrosia Lake in New Mexico, and Gas Hills area of Wyoming were treated in the acid leach - CCD - ion exchange column pilot plant. Mills using this recovery method are now located at Uravan, Colorado, east of Riverton, Wyoming, and at Ford, Washington.

Solvent extraction studies at the Pilot Plant included development work on the Eluex process; studies on equipment design and process flowrates in external and internal mixer-settler units and pulse columns, evaluation of amines and organic - phosphoric acids, and techniques for control of molybdenum. The combined research effort on solvent extraction of uranium from leach liquors by the several A.E.C. research contractors and independent research organizations resulted in a trend to this recovery method in a large number of the more recently built uranium mills. Mills using solvent extraction are located at Shiprock and Grants, New Mexico; Grand Junction, Gunnison, Rifle, and Durango, Colorado; Mexican Hat and Salt Lake City, Utah; Riverton, Wyoming; and Lakeview, Oregon. As mentioned previously, the Edgemont, South Dakota, mill uses solvent extraction in connection with the Eluex process.

A major effort at the Pilot Plant during 1957 was the testing and development of a flowsheet for the recovery of uranium from the lignites of North and South Dakota. Nearly 2000 tons of lignite were consumed in these tests and the results established the Dakota lignites as a reserve of uranium which can be exploited when and if future economics warrant. Although the data and techniques developed during the test work have not been incorporated in a mill, they have been used extensively by private industry and the A.E.C. for evaluating the economics of the recovery of uranium from Dakota lignites.

During the course of the operation of the Grand Junction Pilot Plant approximately 30,000 tons of ore from 40 different mines or locations throughout Western United States were tested. Yellow cake production during the period amounted to 138,500 pounds of contained U₃O₈. The analytical laboratory at Grand Junction, which assayed all mill samples except for special determinations made at the Winchester Laboratory, averaged approximately 8000 assays per month. A metallurgical laboratory handled metallurgical problems encountered in the Pilot Plant and performed metallurgical tests which were not practical to do at Winchester. These included leach tests on pilot plant ore shipments when received, screen analyses, settling and filtration tests and evaluation of mill flocculents, ion exchange loading and elution tests, solvent shakeout tests, and precipitation studies on mill liquors.

During the past year a field office has been maintained at Grand Junction in connection with studies on the radioactive decontamination of uranium mill tailings. Work of this office included sampling tailings from the commercial mills, sampling programs in a group of mills using different flowsheets for the purpose of making radium and thorium balances around these mills, and pilot plant decontamination tests to evaluate methods developed at Winchester.

Mill Assistance

In the course of the project technical assistance was given to uranium mills in Australia, South Africa, Canada, and the Belgian Congo. Engineers and chemists from the Raw Materials Development Laboratory spent considerable time at various individual mills in these countries assisting with leaching, ion exchange, and analytical problems.

During the period that many new uranium mills were being built in the United States and technical, operating, and analytical personnel were learning new and quite different techniques, National Lead personnel from the Laboratory and Pilot Plant gave assistance to these companies. Laboratory personnel from most of the new mills went through training programs at either the Winchester or Grand Junction laboratories. These varied from a few days to several weeks and gave the mill analysts a background in uranium assaying and allied determinations.

Several mills sent operating crews to the Pilot Plant to learn established operating techniques, particularly in connection with the resin-in-pulp ion exchange circuit. Pilot plant engineers, chemists, and operators also assisted seven mills during the early weeks of start-up operations. At a time when it was necessary to get new mills into production as quickly and efficiently as possible and at a time when new metallurgical techniques such as ion exchange were relatively new in this country, this assistance was considered by the private mills to be very helpful.

As new analytical techniques, particularly in connection with the fluorometric uranium analysis, were developed they were passed on to mill personnel and in many cases Winchester or Grand Junction technicians personally helped change equipment or assisted in the adoption of these techniques.

As a great deal of the technology used in the uranium industry was developed by the raw materials development project, the demand for personnel trained in the laboratory and pilot plant was great. In the final analysis the greatest contribution of the project to the atomic energy program may well have been the large number of technical personnel who were trained on the project.

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DESCRIPTION OF FACILITIES

Winchester Laboratory

The research facilities of the Raw Materials Development Laboratory were located at Winchester, Massachusetts, a residential community about 15 miles from Boston. The laboratory building, constructed in 1952, is a modern, single-story, cement block and brick building with a floor area of 31,400 square feet (Figure 1). The building was divided into approximately thirty laboratories, work areas, shops and offices and was equipped and staffed for conducting a wide variety of metallurgical, chemical and analytical investigations. Figure 3 shows a floor plan of the laboratory. A small test plant was available for continuous unit process testing. Well equipped machine and instrument shops provided for the maintenance and construction of standard and specialized equipment.

The laboratory was divided into three departments: Metallurgical, Chemical, and Analytical. The laboratory was equipped for investigations into acid and alkaline leaching techniques, ion exchange, solvent extraction, and precipitation processes. Facilities were also available for conducting mineralogical studies, flotation, gravity concentration, magnetic and electrostatic separations. A well equipped crushing and sampling laboratory assured careful preparation and sampling of the ores received for testing. Figure 4 and 5 show the mineral dressing laboratory and the sample preparation room, respectively.

The analytical facilities contained besides the usual equipment for wet-chemical analyses a complete emission spectrograph laboratory, spectrophotometers and polarographs of both the recording and non-recording types, radiometric counting equipment, and other modern analytical instruments. Figures 6 through 9 show views of some of the chemical and analytical facilities.

Grand Junction Pilot Plant

The Grand Junction Pilot Plant was located at the south end of the A.E.C. Compound on the bank of the Gunnison River. It included two large mill buildings, a crushing and sampling plant building, office and laboratory building, warehouse, maintenance shop, and the necessary areas for stockpiling ore and tailings pond (Figure 2). The Pilot Plant contained, wherever possible, standard types and sizes of equipment so as to minimize the problem of scale-up so commonly encountered in translating the data obtained from pilot plants to full-scale operating plants. The Pilot Plant contained a feed preparation plant where the ores were weighed, crushed, sampled, and stored and four primary leaching and processing circuits;



Figure 1. Raw Materials Development Laboratory Holton Street, Winchester, Mass.



Figure 2. Raw Materials Pilot Plant AEC Compound, Grand Junction, Colo.





WIN-115 - 17 -

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Figure 4. Ore testing laboratory



Figure 5. Sample preparation room







Figure 6. Low-U Laboratory Figure 8. High-U Laboratory



- Figure 7. Fluorometric Laboratory
- Figure 9. Analytical Laboratory

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carbonate leach - filtration, carbonate leach - resin-in-pulp, acid leach - resin-in-pulp, and acid leach - CCD - column ion exchange or solvent extraction.

The carbonate leaching circuits provided for the study of leaching by means of mechanical or air agitation at either atmospheric or elevated pressures. The acid leaching circuits were also equipped for mechanical or air agitation. Recovery of uranium in the acid circuits was accomplished by the resin-in-pulp process or by column ion exchange or solvent extraction from clear solutions obtained by the use of thickeners or filters or combinations of the two. The solvent extraction circuits included both mixer settlers and pulse columns. Auxiliary milling and processing equipment included a flotation circuit and a FluoSolids roaster, as well as miscellaneous tanks, agitators, and filters. A well equipped Analytical Department performed the large number of assays required in the operation of the various circuits, and a metallurgical laboratory conducted metallurgical research and process development studies connected with the operation of the pilot plant.

Views of the interior of the Pilot Plant are shown in Figures 10 through 13. Flowsheets of various circuits are presented in Figures 14 through 19.



Figure 10. Solvent extraction pilot plant Figure 11. Alkaline leaching autoclave





Figure 12. RIP Pilot Plant



Figure 13. Pilot Plant Filtration Circuit

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Figure 14



WIN-115 - 23 -



Figure 16



Figure 17

WIN-115 - 24 -





Figures 18 and 19

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PERSONNEL

The program was initiated in July 1954 under the direction of J. S. Breitenstein, Technical Director. Mr. C. K. McArthur became Technical director in July 1957. The technical operation of the Winchester Laboratory was directed by R. J. Woody and the Grand Junction Pilot Plant was managed, in order, by R. F. Hollis, C. K. McArthur, and R. G. Beverly. The two units operated essentially as distinct facilities with close liaison maintaining a coordinated approach to the technical problems. Dr. M. A. DeSesa was Head of the Analytical Section of the Winchester Laboratory, G. W. Clevenger and D. R. George headed the Metallurgy Department, and Dr. A. M. Ross and H. J. Petrow were in charge of the Chemical Department. Department heads at the Grand Junction Pilot Plant included J. Q. Jones, A. W. Griffith, J. N. Kalahar, J. D. Crozier, and W. D. Charles.

Presented in Figures 20 and 21 are the organization charts as they appeared in January 1, 1955 and January 1, 1958.









WIN-115 - 27 -

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Winchester Laboratory

AEC Case Number	Contractor's Number	Inventor (s)	Title	Disposition
-	WIN-P-1	R. J. Woody	Apparatus for Continuous Countercurrent Ion Exchange	Disclosure inactivated at Winchester
s-13,8 28	WIN-P-2	H. G. Petrow	Process for Recovery and Concentration of Uranium	S.N 626,834. Advised by AEC that prior art interferes
s-14,8 79	WIN-P-3	P. Galvanek, Jr.	A Solvent Leaching Process for the Recovery and Concentration of Uranium	U. S. Patent issued on 2/24/59 - No. 2,875,023.
s-13,8 26	WIN-P-4	F. A. Centanni	Flux for Use in the Fluorimetric Determination of Uranium	Subject material handled by Technical Publication with AEC approval
8-1 5,515	WIN-P-5	R. J. Woody	An integrated Recycle Process for the Recovery of Uranium from Ores	Disclosure submitted to AEC
S-15,981	WIN-P-6	H. F. Wilson	Alkaline Ion Exchange Process for Re- covery of Uranium and Vanadium	U. S. Patent issued on 7/1/58 - No. 2,841,468
s-16, 345	WIN-P-7	P. Galvanek	Multiple Discharge Pump	Advised by AEC that prior art interferes - no filing action
-	WIN-P-8	H. G. Petrow	Uranium Recovery Process (Eluex Process)	Disclosure inactivated at Winchester
-	WIN-P-9	R. J. Woody	Ion Exchange Process	Disclosure inactivated at Winchester

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Summary of Disposition of Invention Reports Winchester Laboratory (Cont'd)

AEC Case Number	Contractor's Number	Inventor (s)	Title	Disposition
S-16, 460	WIN-P-10	P. J. Magno and M. A. DeSesa	Carbonate Oxidants	Disclosure submitted to AEC
s-1 6,468	WIN-P-11	R. J. Woody, F. A. Howland, and E. T. Hollis	Continuous IX Column	Advised by AEC that no filing action will be taken
-	WIN-P-12	W. D. Charles	Uranium Recovery Process	Disclosures inactivated at Winchester
-	WIN-P-13	B. W. Wessling	Apparatus for Continuous Uranium Analysis	Disclosure inactivated at Winchester
-	WIN-P-14	L. Newman	Preparation of UF_{4}	Disclosure inactivated at Winchester
s-16, 594	WIN-P-15	R. J. Allen and H. G. Petrow	Process for UF_4 Production	Application filed by AEC, S. N. 801,977 (48)
S-18, 066	WIN-P-16	J. T. Lynch	Electrolytic Oxidation Method	Advised by AEC that no filing action will be taken

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<u>APPENDIX</u>

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Table 1

Classification of Topical Reports by Subject

July 1, 1954 - June 30, 1959

Symbol		Subject	Topical WIN No.
A	-	Acid leaching, theoretical studies	3, 29
В	-	Acid leaching, plant amenability tests	5, 12, 18, 23, 32, 35, 40, 42, 44, 47, 60, 69, 70, 72, 76, 78
С	-	Alkaline leaching, theoretical studies	3, 73, 89, 103, 104
D	-	Alkaline leaching, plant amenability tests	19, 20, 39, 45, 57, 66, 67, 77, 79, 80, 82, 83, 84, 106, 107, 108, 109, 110
E	- '	Alkaline leaching oxidants	86
F	-	Laboratory ion exchange studies, acid liquors	4, 9, 15, 26, 27
G	-	Laboratory ion exchange studies, alkaline liquors	88
н	-	Ion exchange column test work	26, 44, 76 , 78, 84, 109
I	-	Acid RIP tests	5, 12, 18, 23, 32, 35, 40, 42, 47, 60, 70, 78
J	-	Alkaline RIP tests	11, 17, 39, 77, 82, 83, 88
K	-	Eluex process	28,75
L	-	Laboratory solvent extraction studies	24, 28, 30, 54, 61
M	-	Pilot plant solvent extraction tests	69, 72, 81
N	-	Uranium precipitation	13, 16, 21
0	-	Laboratory ore amenability tests	1, 3, 6, 8, 14, 25, 36, 38, 41, 49, 50, 51, 54, 56, 58, 59, 64, 65, 68, 71, 74, 87, 91, 92, 96, 97
P	-	Analytical, uranium	34, 43, 46 , 63
Q	-	Analytical, nonuranium	7, 10, 52 , 62, 85
R	-	Flotation	2
S	-	Molybdenum	27, 48, 53
Т	-	Vanadium	16, 55
U	-	Solvent leaching	31, 100
V	-	Roasting	54, 81
W	-	Lignites and coals	33, 54, 81
X	-	Ammonia carbonate leaching	37
Y	-	Green salt (UF4)	90, 95
Z	-	Pollution, chemical and radioactive	99, 101, 111, 112, 113, 114
a	-	Countercurrent RIP	102, 105
b c	-	Uranium recovery from tails and scrap Higgins contactor	22, 98
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Uranium Ores Tested with Topical and Progress Report References

July 1, 1954 - June 30, 1959

Ore and Location	Report No. WIN-	Monthly Progress Reports 1/
Ambrosia Lake, New Mexico	56, 60, 64, 67, 72, 76, 84, 107, 108, 109, 110	2-9, 11, 12/56, 1-2-3-10-11-12/57, 1-5/58
Arrowhead, Arizona	18	12/54, 1-2-3-4-5-7/55
Atascosa County, Texas	58	11-12/55
Austin Lignite, Texas		7/56
Blind River, Canada		7-8/54
Bog Type, California		5-6/56
Cal-Uranium, Utah	6, 12	9-10-11-12/54, 2/55
Columbian Samples, So. America		12/56
Copper City Mill Tail, Arizona		12/54
Cord, E. L., Jen-Jackie Claim, Utah	59	12/56, 1/57
Dakota Lignites	54, 81	2/34, 1, 2, 4-12/35, 1-11/36, 1-11/3/
Dominion Reels, So. Airica	50	0/04
Durart Shaft New Merico	JO 60 67 73 76 84	2-3/3/ 3-4-6-7-8-10/56 1-3-3-4-12/57
Dysons' Pum Jungle Australia	00, 07, 72, 70, 04	7-9-9-10-11-19/5/ 9-3-4-5-6-8/55 5/57
Edgement So Bakota	5 14	9-10-11-12/54
Four Corners Utah	40.51	11-12/55. 1/56
Cas Hills. Wyoming	41, 44, 65, 79, 80, 97	12/55, 1/56, 1-2-5-6/57
Globe, Arizona		7-8-11/56, 6/57
Globe Mining Co., Gas Hills, Wyoming	79.80.97	3-6-7/57
Happy Jack Mine. Utah	69	7/54, 9-10-11-12/56, 1/57
Hecla Mining Co., Utah	66	12/55. 1/56
Hidden Splendor Mine, Utah	32	3-4-5-6-7-8-9/55
Holly Minerals Co. (Sec. 14), New Mexico	84, 108, 109	11/57, 1-2-3-4-5/58
Homestake North Alice, Utah	68	1-2-3/57
Homestake (Sec. 32), New Mexico	107	2/58
Jack Pile Mine, New Mexico	3	7-8-9-10/54
Karnes County, Texas	58	7-8/55, 9-10-11 -12/56, 2/5 7
LaBajada, New Mexico	91	2-4-7-8/57
Lakeview Mining Co., Lucky Lass and	30, 74, 78	7-9-10-11-12/56, 3-4-5-6-7-9-10-12/5 7
White King Claims, Oregon		
LaSalle, Colorado		7-8-9/54
La Sal, Utah	20, 39, 45, 73, 77, 112	2, 3, 4, 6-11/55, 9-12/56, 1-7-8-12/57, 1/58
Lehigh Coal and Navigation, Pa.	33	
Little Beaver, Utah	11, 38	12/54, 1-3-5/55
Little Man Claim, Wyoming	JO 22 25	3-3-0/33 2 2 4 5 4 7/55 2/50
Los ochos, Gunnison Mining Co., Colo.	23, 23 //. 25	2-3-4-3-0-//33, 3/30 19/55 1_9_6_5/64 4/80
Mellingkrodt-African Matele Besidue	44 , 0 2	11/54 1-2/55
Maturalo Utob	22	3-/-5-6/55
Mess Top New Merico	47 77	2-3-4-7-8-9/56 1-2-10/57
Midnight Mises Weshington	42.49	6-7-10-11-12/55, 1-2-3/56
Mineral Joe Ores Colorado	50	7-9-10/55, 2-3/56
Monticello Blends. Utah	70. 106	7-8-9/56, 8/57, 1-2/58
Monument Valley, Arizona	83	12/55, 1-2/56
Moonlight Claim, Utah	87	11-12/56, 1/57
Mount Isa District, Australia		3-4-5-6-10-11-12/55
Ottawa Athabasca, Canada		7/54, 8/54
Phillips Petroleum Co. (Sec. 28), New Mex.	110	11-12/56, 4-5-6/58
Poison Canyon, New Mexico		8-9-10/56
Pryor Mountain, Wyoming	41	4/56
Riverton Ore Samples, Wyoming	97	9-10/55, 3/56, 6/57, 1-2/58
Refinery Slags, Mallinckrodt and Fernald	98	3-4-5-6-7-8-9/57, 1-4/58
Saint Anthony Uranium Corp., New Mexico	96	7-8-9/57
Schwartzwalder, Ralston Creek, Colorado	71	6-7-9-10-11-12/55, 9-10/56, 2-3/58
Todilto Limestone, New Mexico	57, 77, 112	1-3/55, 3-4-5-6-7-12/56, 1/57
U & I Aimar, Utah	00 82	12/33, 1-2-3/30 0-10-11/57
Uranium Reduction Co., Utah	84	9+10-11/3/ 9/5/ 3 0 0 11/55 5/57
View, Utah Namuna Chaun Chaun Carrier h Mark	2, IL, 29, 39, 82 51	0/24, 3-8-9-11/33, 3/36 11_12/55
venuta Group (rour Corners), Utan Vitro Huoming	80	1/57 9/58
Vestern Cold and Uranium Co. Arisono	8	10-11-12/54
White Canvon Utah	35. 69	10-11-12/55, 2-3/56, 6/58
Whites' Rum Jungle, Ametralis		5-7/56
Woodrow Ore. New Mexico		7/55
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1. 2, 3, 4/56 refers to February, March, and April Monthly Progress Reports, 1956, etc.

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Table 3

Contents of Monthly Progress Reports Classified by Subject Symbols

Subject Symbol Month 1/ A B C D E F <u>GHIJKLMNOPQRSTUVWX</u> YZAbc 7/54 х х х х 8/54 x х х x х х 9/54 x x х x х 10/54 x х х х х 11/54 х х х х х x х x x 12/54 x x x х x х х х х х 1/55 х х х х х х х x х 2/55 х х x х х х x х x 3/55 х х х х х х хх х х x 4/55 х х .. **X** х x х x х х х х х x x 5/55 х х x х х х х х х x x x 6/55 х х х х хх х х x х x х X 7/55 х х х х х x x х x х х х x х х x 8/55 х х х х х х х х х х x 9/55 x х x х х х х хх х х х х x 10/55 х х х х х х х хх х x х х X 11/55 х х х х х х х х х хх х х хх х 12/55 x х х х х x x х х x x x 1/56 x х х х x x х х хх x хх х 2/56 х х х х х х х х х х х х x x x 3/56 х x х х х x х х х х х x x х 4/56 х х х хх х х х x х х х х х x x 5/56 х хх х х x х x х х х x х 6/56 х хх х х х х хх х х х x x х 7/56 х х х х х х x х х х х х х x x 8/56 х x х х хх х х х х x х x х x 9/56 х $\mathbf{x} \sim \mathbf{x}$ х х x х х х х х х х х x x x 10/56 х х х х x x x х х х x х x 11/56 х x х х х x х х х х х х х х x 12/56 х х х х х х хх х х х x х х x х x 1/57 х х х х х х х х х х х x х х х x 2/57 х х х х x х х х х х х х X 3/57 х x х хx х х x х х x х x x x 4/57 x х х х x х х х хх х х х x x х x 5/57 х х х х х х х х х х х х х х х x x х x x 6/57 х х х х х х х х х х х х х х x х х х х 7/57 х х х х х х х х х х х х x 8/57 х x х x x х х х х х x x х 9/57 х х х х х х х х х х х х x x 10/57 х х х х х х х х х 11/57 х х х х х х х х х х x x х 12/57 х x х х x х х х х х x 1/58 х х x x х х х x х x x x х 2/58 х х x х х х х х х 3/58 х х x x х х х х х х x х х 4/58 х х х х x х х х x x x 5/58 х х х х х х х х x 6/58 х хх x х х х х 7/58 x х 8/58 х 9/58 ×, х 10/58 х 11/58 х х 12/58 x

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July 1, 1954 - June 30, 1959

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NATIONAL LEAD COMPANY, INC. Raw Materials Development Laboratory

ABSTRACTS OF REPORTS

WIN-1

HARMONY ORE. J. T. Lynch. October 13, 1954. 14 p.

A sample of ore from the Harmony Mines, Union of South Africa, assaying 0.042% U308 was studied to compare leaching methods and to make a preliminary study of resin poisoning. Extraction of 89.7% of the uranium was obtained by two stage cyclic leaching with 28 pounds of H2SO4 and 9 pounds of 85% MnO2 per ton of ore. Best extraction of the uranium obtained by single stage leaching was 84.8% with reagent requirements of 33 pounds of H2SO4 and 9 pounds of 85% MnO2 per ton of ore. After 13 loadings on IRA-400 resin using pregnant solution obtained from two stage cyclic leaching, only a trace of cobalt was found on the resin.

WIN-2

FLOTATION AND LEACHING OF PRODUCTS FROM HIGH LIME UTEX ORES. D. R. George and R. A. Eisenhauer. December 31, 1954. 29 p.

Test data are presented on the flotation of calcite from high lime Utex ores and on leaching of the products with sulfuric acid or sodium carbonate solutions.

WIN-3

ACID AND CARBONATE LEACHING OF NORTH JACKPILE ORE. J. Q. Jones, J. B. Larson, J. T. Lynch, E. S. Porter, G. Trueman and H. I. Viklund. February 21, 1955. 21 p.

Laboratory investigation of a composited drill core sample from the North Jackpile ore body near Grants, New Mexico, revealed that the ore is readily amenable to acid leaching and ion exchange. Good settling rates were obtained on neutral and acid leached pulps. An oxidant was beneficial to leaching. Carbonate leaching was also effective either with a chemical oxidant or following a preliminary roast. Filtration of carbonate leached pulps was difficult.

ION EXCHANGE RESIN TESTING. F. Pickwick, Jr. November, 1954. 32 p.

This report deals with the testing of resin manufactured by the Rohm & Haas Company. Data obtained in test work performed between February 1952 and November 1954 are presented.

WIN-5

RESIN-IN-PULP PILOT PLANT TESTING OF EDGEMONT ORE. R. Hollis, C. K. McArthur, T. F. Izzo, A. W. Griffith and R. L. Shimmin. January 11, 1955. 23 p.

Ore from the Edgemont District of South Dakota was treated in the Resin-in-Pulp Pilot Plant. Satisfactory leaching was accomplished with about 40 pounds of sulfuric acid per ton of ore. Leach contact times of 10, 8, and 6 hours all yielded extractions of 97% of the uranium. No difficulty was encountered in ion-exchanging this liquor. Recovery in the adsorption units was over 99%. A solution 0.9M NO3 with the pH adjusted to 1.2 with sulfuric acid was employed as the eluant. Pregnant eluate was precipitated with MgO resulting in a product that averaged 67.40% U308. Calculated recovery was 95.7%.

WIN-6

CARBONATE LEACHING, ACID LEACHING, SETTLING, AND ION EXCHANGE TESTING OF CAL-URANIUM ORE. D. R. George, J. B. Larson, E. S. Porter, and H. I. Viklund. October 3, 1955. 37 p.

The results of acid and carbonate leaching tests, ion exchange tests of acid leach solutions, thickening tests of acid leached pulps, cyclic carbonate leaching tests, and filtration tests of carbonate leached pulps are described.

WIN-7

THE SPECTROPHOTOMETRIC DETERMINATION OF PHOSPHORUS AS MOLYBDO-VANADOPHOSPHORIC ACID. K. P. Quinlan and M. A. DeSesa. February 21, 1955. 21 p.

The molybdovanadophosphoric acid method for the spectrophotometric determination of phosphorus has been extensively re-

WIN-7 (Continued)

viewed. The optimum concentrations of acid, vanadium (V), and molybdenum (VI) were determined by factorial experiment. The optimum color development occurs in solutions which are 0.4<u>M</u> in acid, 0.02 to 0.06<u>M</u> molybdenum (VI) and 1.0 to 4.0<u>mM</u> vanadium (V). The optimum range is 3 to 20 ppm P₂O₅ for 1 cm cells. Dichromate is the only serious interference, but can be eliminated by volatilization of the chromium as chromyl chloride.

WIN-8

PHELIMINARY LEACHING AND ION EXCHANGE STUDIES OF A SAMPLE OF WESTERN GOLD AND URANIUM COMPANY ORE. J. T. Lynch and H. I. Viklund. July 16, 1956. 16 p.

A sample of ore from Western Gold and Uranium Company properties in Arizona, assaying 0.217 per cent U_308 , was studied to determine leaching and ion exchange data. Acid requirements employing various leaching procedures and uranium ion exchange loading using different manufacturer's resin are presented. Some data are also presented on carbonate leaching.

WIN-9

MISCELLANEOUS ELUTION STUDIES. A. R. Kazanjian. March 5, 1956. 27 p.

An investigation was made of the variables involved in a 5M NaCl - H2O elution scheme. The most promising procedure was used in a cyclic ion exchange system. Studies were also made on the effect of iron to phosphate ratios on uranium ion exchange and the effect of temperature on elution.

WIN-10

THE SPECTROPHOTOMETRIC DETERMINATION OF TETRATHIONATE. O. A. Nietzel and M. A. DeSesa. April 18, 1955. 18 p.

The spectrophotometric method of Robinson for the determination of tetrathionate has been modified to yield a procedure of greater sensitivity and accuracy. The procedure depends on conversion of tetrathionate to thiocyanate and determination of the thiocyanate formed with an excess of ferric iron. By developing the color in opaque cylinders, the rapid decomposition of the WIN-10 (Continued)

ferric thiocyanate color has been eliminated for all practical purposes. The use of ferric nitrate and nitric acid instead of ferric chloride and hydrochloric acid has decreased the optical density of the reagent blanks. The optimum concentrations of reagents have been evaluated. By measuring the final color at 460 mµ instead of at 525 mµ a two fold increase in sensitivity has been achieved. A rapid, accurate procedure is presented for analyzing liquors containing as little as 0.002 gram of tetrathionate per liter.

WIN-11

PRELIMINARY PILOT PLANT TESTING OF RESIN-IN-PULP ION EX-CHANGE OF ALKALINE LEACH PULPS. C. K. McArthur, T. F. Izzo, R. G. Beverly, A. W. Griffith and R. L. Shimmin. April 25, 1955. 21 p.

To determine the possibility of recovering uranium from alkaline leach pulps, Utex ore from Stockpile 33 at Monticello, Utah was treated in the Resin-in-Pulp Pilot Plant circuits. From the test work a tentative alkaline Resin-in-Pulp Pilot Plant flowsheet was established. Data are presented on the recovery by adsorption units as well as information on the elution and precipitation of uranium concentrate.

WIN-12

RESIN-IN-PULP PILOT PLANT TESTING OF CAL-URANIUM ORE. C. K. McArthur, A. W. Griffith, T. F. Izzo, R. G. Beverly and R. L. Shimmin. April 29, 1955. 19 p.

Cal-Uranium ore from the Lisbon Valley District of Utah was treated in the Resin-In-Pulp Pilot Plant from November 21 to December 19, 1954. The average grade of the ore as treated was 0.14% U308 with an average lime content of 9.6%. The leaching was accomplished with an average consumption of 345 lb of sulfuric acid per ton of ore. Leach contact times of 18, 14, and 10 hours yielded leach extractions of 95.5, 92.9, and 92.8%, respectively. One leach of 10 hours contact time with the addition of 5 lb MnO2 per ton of ore resulted in an extraction of 94.8%. Some difficulty was encountered in ion exchanging this liquor. Recovery in the adsorption units was 97.8%. The eluant used was 0.9M NO3 adjusted to a pH 1.2 with H2SO4. The precipitant used was MgO which gave a final product of 57.8% U308. Calculated recovery was 90.13%.

URANIUM RECOVERY BY HYDROGEN REDUCTION OF CARBONATE LEACH LIQUORS. H. Papazian. November 1, 1955. 25 p.

The application of hydrogen reduction in the presence of a nickel catalyst for the recovery of uranium from carbonate liquors has been investigated. Tests were conducted on a laboratory scale in batch and continuous operations.

WIN-14

LABORATORY INVESTIGATION OF EDGEMONT SANDSTONE ORE. G. Trueman, H. I. Viklund, J. B. Larson and P. N. Thomas April 18, 1955. 33 p.

Laboratory investigations were made of a sample of sandstone-type uranium ore from Edgemont, South Dakota. The amenability of the ore to acid and carbonate leaching was studied as well as methods of recovering the uranium from leach solutions.

WIN-15

ION EXCHANGE RESIN TESTING - PART II PERMUTIT RESINS TESTED DURING THE PERIOD FEBRUARY 1952 THROUGH NOVEMBER 1954. F. Pickwick, Jr. November 15, 1955. 30 p.

This report presents the results of test work performed on samples of ion exchange resins submitted by The Permutit Company to this laboratory for evaluation in the period February 1952 through November 1954. During this period, the uranium adsorption and elution properties of the Permutit resins have been observed to improve considerably. By using early test data, The Permutit Company was able to adjust the manufacture of their resins so that later resin lots showed improved uranium adsorption and elution properties.

WIN-16

PRECIPITATION OF URANIUM AND VANADIUM FROM CARBONATE LEACH LIQUORS USING SODIUM AMALGAM. H. E. Dixon. September 20, 1955. 32 p.

Basic equipment design, results of laboratory test work, and a partial economic analysis of the sodium-amalgam precipitation and reduction process as applied to carbonate leach solutions are presented.

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WIN-17

INITIAL OPERATION OF NEW ACID LEACH RESIN-IN-PULP PILOT PLANT. C. K. McArthur, T. F. Izzo and R. L. Shimmin. July 5, 1955. 28 p.

The components and operation of the new acid leach Resin-in-Pulp (RIP) Pilot Plant and the results of a shakedown run are described. The new fourteen bank system proved to be practical in operation and highly efficient for uranium recovery from desanded ore pulps.

WIN-18

RESIN-IN-PULP PILOT PLANT TESTING OF ARROWHEAD ORE. C. K. McArthur, T. F. Izzo, and R. L. Shimmin. May 23, 1955. 30 p.

Arrowhead ore from the Cameron district of Arizona was successfully treated in the Resin-In-Pulp Pilot Plant. Leach extraction with the use of 205 pounds of H_2SO_4 and 10 pounds of MnO_2 per ton of feed averaged 95.74 per cent. Ion exchange recovery averaged 99 per cent of the uranium in solution with nine banks of resin on exhaustion. The eluting solution used for the majority of the test period was 0.9 M NH₄NO₃ adjusted with H_2SO_4 to a pH of 1.2. The product from nitrate elution averaged 75.7

WIN-19

DESCRIPTION OF ALKALINE LEACH PILOT PLANT AT GRAND JUNCTION, COLORADO J. Q. Jones, D. O. Skiles, and G. Winslow. June 24, 1955. 13 p.

The pilot plant facilities at Grand Junction, Colorado, for testing the amenability of domestic uranium ores to the carbonate leaching process are described. The chemistry of uranium dissolution in carbonate solutions and its precipitation with NaOH is discussed briefly.

WIN-20

INITIAL TESTS OF LASAL SHAFT ORE IN THE ALKALINE LEACH PILOT PLANT. J. Q. Jones, D. O. Skiles, and G. Winslow. July 29, 1955. 26 p.

Initial testing of LaSal ore in the Alkaline Leach Pilot Plant at Grand Junction, Colorado, took place during the period February 15 to March 7, 1955. By the use of an extended leaching time of 112 hours and a temperature of $172^{\circ}F$, a dissolution of 99.1 per cent of the uranium was obtained. Three-stage filtration of the pulp gave a soluble loss of 1.5 per cent and a filter rate of 276 pounds per square foot per 24 hours, using 0.05 pound of Separan-2610 per ton. The best filter rate obtained was in excess of 600 pounds per square foot per 24 hours. Overall recovery of uranium in the "yellow cake" was 95.7 per cent for the entire run. The product assayed 75.5 per cent on a dry basis, and slightly better than 80 per cent U₃O8 if washed on the filter before drying. Indicated reagent consumptions are 20 pounds of caustic soda and 0.1 pound of Separan per ton of ore. Fuel oil requirements for pulp heating were 21.3 gallons per ton of ore.

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WIN-21

ELECTROLYTIC STUDIES IN CARBONATE SOLUTIONS. A. R. Kazanjian. April 4, 1956. 23 p.

The electrolytic reduction and precipitation of uranium from carbonate leach solutions was investigated. Electrolytic reduction of uranium in a mercury cathode cell followed by precipitation with sodium hydroxide was also studied.

WIN-22

RECOVERY OF URANIUM, COBALT, NICKEL AND COPPER FROM AM-7 RESIDUES. D. R. George. July 6, 1955. 29 p.

The results of laboratory investigations for the recovery of uranium, cobalt, nickel, and copper are presented. The test work includes sodium carbonate leaching, sulfuric acid leaching, ion exchange testing, and cobalt, nickel, and copper precipitation studies.

WIN-23

RESIN-IN-PULP PILOT PLANT TESTING OF LOS OCHOS ORE. C. K. McArthur, A. W. Griffith, R. W. Shimmin. October 15, 1955. 30 p.

During the months of April through June of 1955, Los Ochos ore from the Gunnison area of Colorado was treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado. The report presents detailed information on leaching, ion exchange, and precipitation in connection with the processing of this ore. Results showed that the ore is very amenable to the process and that relatively low acid consumption was required for good uranium extraction.

WIN-24

THE RECOVERY OF URANIUM FROM SULFATE LEACH LIQUORS BY THE TBP-THIOCYANATE PROCESS. H. G. Petrow and H. N. Marenburg. November 7, 1955. 17 p.

A process for the solvent extraction of uranium from clear sulfate leach liquors has been developed. The uranium is extracted into a tributyl phosphate-kerosene solvent as uranyl thiocyanate. The extracted uranyl thiocyanate is re-extracted into aqueous sodium carbonate. Laboratory data indicate the process to be economically applicable to plateau ores.

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WIN-25

LABORATORY INVESTIGATION OF THORNBURG LOS OCHOS ORE. E. S. Porter, P. N. Thomas, H. I. Viklund and G. Trueman. October 17, 1955. 31 p.

Laboratory investigations were made of three samples of uranium ore from the Los Ochos lease of the Thornburg Mining Company. The amenability of the ore to acid and carbonate leaching was studied as well as methods of recovering the uranium from acid leach solutions.

WIN-26

THE RECOVERY OF URANIUM FROM ORE PULPS USING FIXED ION EXCHANGE RESIN BEDS. G. W. Clevenger and J. T. Lynch. December 21, 1955. 25 p.

The development of new techniques which enable an ore pulp to pass through fixed ion exchange resin beds for the recovery of dissolved values is described. Data are given for the recovery of uranium from various ore pulps in an ll-inch diameter pilot plant column.

WIN-27

DEVELOPMENT OF AN EFFICIENT ELUANT FOR REMOVAL OF MOLYBDENUM FROM ANION EXCHANGE RESINS. K. P. Quinlan and R. J. Barry. August 1, 1956. 21 p.

The poisoning of anion exchange resins by molybdenum adsorption has been briefly studied. Although no satisfactory method was found to prevent the adsorption of molybdenum from pregnant leach liquors, an effective eluant for molybdenum was developed which is superior to the 5-10% sodium hydroxide solutions previously used for this purpose. It was found that the presence of small quantities of a good displacing ion such as chloride or nitrate in dilute solutions of sodium or ammonium hydroxide greatly increases the speed and efficiency of molybdenum removal. Investigations also revealed that by the addition of 0.5 per cent sodium or ammonium hydroxide, RIP barren eluate bleed can be used effectively as an eluant for molybdenum.

WIN-28

SOLVENT EXTRACTION OF URANIUM FROM SULFURIC ACID ELUATES. H. G. Petrow, K. P. Quinlan, H. N. Marenburg and J. Apidianakis. March 29, 1956. 16 p.

A process for the elution of uranium from loaded Amberlite XE-123 resin with sulfuric acid, and the subsequent recovery of the uranium from the pregnant eluate by solvent extraction has been devised. The process eliminates many of the difficulties accompanying both nitrate and chloride elution, and in an RIP system, indicates a lower chemical cost than with either nitrate or chloride elution.

STUDIES OF THE EFFECTS OF VARIOUS TYPES OF AGITATION ON THE EXTRACTION OF URANIUM FROM A SAMPLE OF UTEX ORE. P. N. Thomas. December 1, 1955. 41 p.

Test data are presented showing the effects of various types of agitation on the extraction of uranium by acid leaching Utex Sample 75-7.

WIN-30

RECOVERY OF URANIUM FROM LAKEVIEW LEACH LIQUOR USING TRI-LAURYLAMINE. O. A. Nietzel, C. F. Lubinger and J. Apidianakis. September 11, 1957. 14 p.

An economical recovery of uranium from Lakeview leach liquor was obtained with a solvent extraction technique using trilaurylamine as the uranium extractant.

WIN-31

A SOLVENT LEACHING PROCESS FOR THE PRODUCTION OF HIGH-PURITY URANIUM PRODUCTS DIRECTLY FROM LOW-GRADE ORES. P. Galvanek, Jr. and M. S. Pelland. December 9, 1955. 22 p.

A solvent leaching process is described in which an organic solvent, consisting of 5 volume per cent tributyl phosphate and 95 volume per cent kerosene, is used to selectively leach uranium directly from nitrate-conditioned, acid-cured, low-grade ores. Filtration and other clarification operations common to most ore treatment processes are eliminated. The process has been tested on several Colorado Plateau ores, both primary and secondary, yielding overall uranium recoveries ranging from 92 to 98 per cent. A uranium product analyzing over 99 per cent U₃O8 is produced.

WIN-32

RESIN-IN-PULP PILOT PLANT TESTING OF HIDDEN SPIENDOR ORES. D. O. Skiles and R. L. Shimmin. January 20, 1956. 50 p.

During the period June 18, 1955 through September 8, 1955, ore from the Delta Mine of the Hidden Splendor Mining Company was treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado. The report presents detailed information on the leaching, ion exchange, and precipitation involved in processing this ore. Results show the ore to be amenable to the Resin-In-Pulp extraction process.

LABORATORY INVESTIGATIONS OF LEHIGH COAL AND NAVIGATION COMPANY ORE. G. Trueman, E. S. Porter and A. R. Kazanjian. March 8, 1956. 19 p.

The results of laboratory tests on a sample of ore from the Lehigh Coal and Navigation Company stockpile at Palmerton, Pennsylvania are described. The test work included acid leaching, filtration and thickening, and recovery of uranium from acid leach solutions by ion exchange.

WIN-34

THE FLUORIMETRIC DETERMINATION OF URANIUM. F. A. Centanni, A. M. Ross and M. A. DeSesa. February 10, 1956. 40 p.

A method evolved from over ten years experience is described for the fluorimetric determination of uranium. This method is especially applicable for laboratories which are planning to install equipment for fluorimetric analysis since the fluorimeter employed is available commercially and the procedure is described in detail. Also reported is a new fluoride flux which is superior in sensitivity, precision, and ease of use to previously employed fluxes.

WIN-35

RESIN-IN-PULP PILOT PLANT TESTING OF WHITE CANYON ORES. J. Q. Jones, W. A. Millsap, T. F. Izzo and R. L. Shimmin. February 13, 1956. 45 p.

During the period of September 15 to November 14, 1955, White Canyon ore from Stockpiles 19 and 35 at Monticello, Utah, was treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado. The ore contained in these stockpiles originally came from the White Canyon area of Utah. The report contains detailed information on grinding, leaching, sand-slime separation, ion exchange, and precipitation in connection with the processing of this ore. Results show the ore to be amenable to the Resin-In-Pulp process.

WIN-36

LABORATORY TESTING OF LITTLE MAN CLAIM ORE. G. Trueman. February 23, 1956. 17 p.

Laboratory studies were made of a sample of ore from the Little Man Claim in Wyoming. The amenability of the ore to acid leaching and ion exchange was investigated as well as the possibility of molybdenum removal by flotation.

SEMI-PILOT OPERATION OF THE AMMONIUM CARBONATE LEACHING PROCESS. E. T. Hollis. February 27, 1956. 29 p.

A process utilizing ammonium carbonate as a lixiviant for uranium and steam stripping as a means of recovery of the values has been tested. Some data are given on both leaching and precipitation aspects of the flowsheet.

WIN-38

AMENABILITY TESTING OF HOMESTAKE LITTLE BEAVER AND RICHARDSON CLAIM ORES. G. Trueman, E. S. Porter, H. I. Viklund and J. B. Larson. September 10, 1956. 31 p.

The results of the laboratory investigation of ore samples from the Little Beaver claim and from the Richardson claim are discussed. Data are presented on carbonate leaching, acid leaching, settling and filtration, and ion exchange of acid liquors.

WIN-39

ALKALINE RESIN-IN-PULP PROCESS FOR THE RECOVERY OF URANIUM FROM ITS ORES. J. Q. Jones, J. G. Roeschlaub, R. L. Shimmin, H. F. Wilson, and H. D. Moulton, Jr. January 19, 1956. 71 p.

During the period May 25, 1955 through August 23, 1955, process development studies were carried out in the Alkaline Leach-RIP Pilot Plant at Grand Junction, Colorado. La Sal ore was used during this time. From September 2, 1955 to November 12, 1955, a special blended sample of Utex ore from the Uranium Reduction Company was treated to determine process amenability for vanadium bearing ores of the type found in the Big Indian Wash district of Utah. The report presents detailed information on the process and its development and on the leaching, ion-exchange, and precipitation involved in the processing of these ores. Results show the process can be applied commercially to the treatment of some uranium ores.

WIN-40

RESIN-IN-PULP PILOT PLANT TESTING OF FOUR CORNERS URANIUM COMPANY ORES. H. F. Wilson, J. Q. Jones and R. L. Shimmin. April 18, 1956. 34 p.

Ores produced by the Four Corners Uranium Company from the Green River District in Utah were treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado during the period from November 14 through December 16, 1955. The report presents detailed information on the leaching, ion exchange, and precipitation involved in processing these ores. Results show the ores to be amenable to the Acid Leach Resin-In-Pulp recovery process.

LABORATORY INVESTIGATION OF PRYOR MOUNTAIN ORE. H. I. Viklund and H. Papazian. September 12, 1956. 18 p.

The results of the laboratory investigation of an ore sample from the Pryor Mountain Area of Montana and Wyoming are presented. Alkaline and acid leaching are discussed and methods are recommended for pilot scale testing.

WIN-42

ACID LEACH RESIN-IN-PULP PILOT PLANT TESTING OF SPOKANE MIDNIGHT ORE. J. Q. Jones, R. G. Beverly and R. L. Shimmin. April 20, 1956. 43 p.

Uranium ore from the Midnight Mines near Spokane, Washington was treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado during the period of December 18, 1955, through January 25, 1956. The report presents detailed information on leaching, ion exchange, and precipitation involved with the processing of the Spokane Midnight ore. Also included are sections on mill design considerations and the results of column ion exchange tests performed at the Winchester Raw Materials Development Laboratory. From the pilot plant test, it was concluded that the ore is amenable to the Acid Leach Resin-In-Pulp Process. Laboratory test work showed the leach liquor exhibited excellent column ion exchange properties.

WIN-43

THE DIRECT SPECTROPHOTOMETRIC DETERMINATION OF URANIUM IN SULFATE AND CARBONATE SOLUTIONS. B. W. Wessling and M. A. DeSesa. June 18, 1956. 12 p.

A spectrophotometric method of analysis for uranium based on the absorption of ultraviolet light by uranyl sulfate and carbonate complexes is described. The method has been used to provide accurate, rapid analyses of uraniferous solutions used in batch and column ion exchange loading tests.

WIN-44

ACID LEACH CCD - COLUMNS PILOT PLANT TESTING OF LUCKY Mc ORE. T. F. Izzo, J. Q. Jones and R. L. Shimmin. May 12, 1956. 64 p.

From January 24 to April 10, 1956, Lucky Mc ore from the Riverton area of Wyoming was treated in the Acid Leach CCD-Columns Pilot Plant at Grand Junction, Colorado. The report contains detailed information on the grinding, leaching, liquid-solid separation by continuous countercurrent decantation, ion exchange, and precipitation in connection with the processing of this ore. A section is included on mill design considerations. Results show the ore to be amenable to the CCD-Columns recovery process.

FINAL REPORT OF THE ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF LASAL ORE. A. W. Griffith, T. F. Izzo, D. O. Skiles and G. Winslow. April 5, 1956. 64 p.

LaSal ore from the Big Indian Wash district of Utah was treated for a second time in the Alkaline Leach - Filtration Pilot Plant at Grand Junction because of a suspected change in ore characteristics as mining progressed. The report contains detailed information on grinding, thickening, leaching, residue filtration, and precipitation. A section on mill design considerations is also included. Results show the ore to be amenable to the Alkaline Leach - Filtration Process.

WIN-46

SPECTROPHOTOMETRIC DETERMINATION OF URANIUM WITH THIOCYANATE IN BUTYL CELLOSOLVE-METHYL ISOBUTYL KETONE-WATER MEDIUM. O. A. Nietzel and M. A. DeSesa. September 6, 1956. 20 p.

A spectrophotometric method for the determination of uranium in ores and leach liquors is presented. This method consists of a separation of uranium from interfering ions by extraction into methyl isobutyl ketone, using aluminum nitrate as a salting agent, followed by development of the color on a portion of the extract with a solution of annonium thiocyanate in a butyl cellosolve-water solvent. The yellow uranyl thiocyanate complex forms immediately, and the color is stable for at least 48 hours. The optimum range of uranium concentration at 375 mµ is from 0.2 to 2.0 grams U_3O_8 per liter in the sample aliquot. The coefficient of variation of absorbance measurements on standard solutions at 375 mµ was found to be $\pm 0.3^4$ per cent. Titanium is the only serious interference but procedures are given which make it possible to analyze samples containing as much as 5 mg of titanium in the sample aliquot.

WIN-47

ACID LEACH RESIN-IN-PULP PILOT PLANT TESTING OF MESA TOP ORE. J. Q. Jones, P. N. Thomas and R. L. Shimmin. May 25, 1956. 38 p.

Mesa Top ore from the Ambrosia Lake district of New Mexico was treated in the Acid Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado, from February 27 to April 6, 1956. This report contains data on the leaching, ion exchange, and precipitation characteristics of that ore. A section on mill design considerations is included. The data show that Mesa Top ore is amenable to the Acid Leach Resin-In-Pulp Process if molybdenum is removed from the resin periodically.

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WIN-48

PRECIPITATION OF MOLYBDENUM FROM ION EXCHANGE FEEDS BY NEUTRALIZATION IN THE PRESENCE OF IRON. P. J. Magno. November 15, 1956. 38 p.

The removal of molybdenum from acid leach liquors by neutralization in the presence of iron has been evaluated as a method of decreasing the concentration of molybdenum to a tolerable level in ion exchange feeds. Such variables as acid concentration, iron to molybdenum ratio, temperature, and concentration of silicate and aluminum in the leach liquor were examined in order to develop the optimum conditions for the precipitation of molybdenum. The precipitation procedure was tested on leach liquors from Ambrosia Lake District Ore and from several lignite ores. Leaching tests made on lignite ores indicate that iron and molybdenum can be precipitated during the leaching by suitable control of the acidity.

WIN-49

LABORATORY INVESTIGATION OF MIDNIGHT MINES ORE. E. S. Porter, E. T. Hollis and H. I. Viklund. December 14, 1956. 24 p.

Laboratory amenability testing was carried out on two samples of ore from the Midnight Mines, Spokane, Washington. Acid leaching, filtration and thickening of neutral and acid pulps, ion exchange of acid liquors, and carbonate leaching are discussed. Results of ion exchange testing of an acid leach liquor from the Grand Junction Pilot Plant are also reported.

WIN-50

LABORATORY INVESTIGATION OF MINERAL JOE ORE. E. S. Porter and H. I. Viklund. January 28, 1957. 26 p.

The results of laboratory testing of two samples of ore from the Mineral Joe Mine in the Jo Dandy Area are presented. A major part of the discussion concerns acid leaching, solid-liquid separation of acid leached pulps and ion exchange of the resulting solutions. Data are also presented on the uranium extraction and reagent consumption by leaching with carbonate solutions. The results of one test on the recovery of vanadium after extracting the uranium are reported.

FOUR CORNERS URANIUM COMPANY ORE. J. B. Breymann, T. J. Sentementes, H. I. Viklund and J. B. Larson. February 1958. 20 p.

Laboratory amenability tests were run on three samples received from Four Corners Uranium Company. The discussion includes acid and carbonate leaching, ion exchange and settling of acid leached pulps.

WIN-52

DETERMINATION OF TRIBUTYL PHOSPHATE. R. J. Allen and M. A. DeSesa. November 15, 1956. 27 p.

Because of the need for a rapid method of analysis for TBP in kerosene and hexane diluents, an investigation into proposed methods of analysis for TBP was made. As a result of this study, the two indirect methods based on the proportional extraction of nitric acid or uranium by solutions of TBP were modified and improved. Also a new, very sensitive, indirect photometric method based on the ultraviolet absorbance of the TBP-uranium complex was developed. In conjunction with an evaluation of the acid saturation method, the successive formation constants for the TBP-nitric acid complexes were determined to be 0.45 for TBP(HNO₃) and 0.039 for TBP(HNO₃)₂.

WIN-53

REMOVAL OF MOLYBDENUM FROM ACID LEACH LIQUORS BY ACTIVATED CARBON. E. T. Hollis and H. E. Dixon. July 29, 1958. 25 p.

Data are presented on the adsorption of molybdenum on activated carbon. The effect of retention time and linear flow on adsorption, the use of sodium hydroxide as an eluant, and the possibility of recovering molybdenum from the caustic eluate are discussed.

WIN-54

LABORATORY INVESTIGATION OF DAKOTA LIGNITES. R. J. Woody, D. R. George, H. Petrow, J. B. Breymann and E. S. Porter. April 1, 1957. 167 p.

This report deals with the laboratory investigation into methods of recovery of uranium from Dakota Lignites. A flowsheet is recommended for pilot plant testing.

WIN-55.

A SPECTROPHOTOMETRIC INVESTIGATION OF VANADIUM(V) SPECIES IN ALKALINE SOLUTIONS. L. Newman, W. J. LaFleur, F. J. Brousaides and A. M. Ross. June 10, 1957. 41 p.

The interpretation of spectrophotometric data has demonstrated that both monohydrogen orthovanadate and pyrovanadate are formed during the first break in the titration of orthovanadate with acid. A constant of 0.097 ± 0.005 has been obtained at 25°C for the hydrolysis of orthovanadate to monohydrogen orthovanadate at an ionic strength of 3.0 for vanadium concentrations of 2×10^{-4} M to 1×10^{-2} M, hydroxide concentrations of 0.01M to 3.0M and wavelengths of 260 mµ to 360 mµ. A constant of 48 ± 5 has been obtained for the dimerization of monohydrogen orthovanadate to pyrovanadate for vanadium concentrations of 0.01M to 0.1M and hydroxide concentrations of 0.0015M to 0.01M.

WIN-56

AMENABILITY TESTING OF AMBROSIA LAKE DISTRICT ORE. H. E. Dixon and H. I. Viklund. January 2, 1958. 62 p.

The results of acid and alkaline amenability tests on 28 samples from the Ambrosia Lake District of New Mexico are presented.

WIN-57

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF TODILTO BLACK LIMESTONE ORE. A. W. Griffith, W. A. Millsap and G. Winslow. December 19, 1956. 37 p.

During the period of February 20 to March 20, 1956, Todilto Black Limestone ore from Stockpile 79 at Grants, New Mexico was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. The ore contained in this stockpile came from the Grants area of New Mexico. The report contains detailed information on grinding, thickening, leaching, filtration, and precipitation in connection with the processing of this ore. Results show the ore to be amenable to the Alkaline Leach - Filtration process.

WIN-58

AMENABILITY TESTING OF ORES FROM KARNES COUNTY AND ADJACENT AREAS IN TEXAS. D. R. George and J. T. Lynch. June 23, 1958. 31 p.

The results of amenability tests on ores from Karnes, Duval, Gonzales and Atascosa Counties in Texas are presented.

LABORATORY INVESTIGATION OF E. L. CORD SAMPLE. E. S. Porter and H. I. Viklund. January 14, 1957. 18 p.

The results of metallurgical tests involving acid and carbonate leaching of a sample of ore from the E. L. Cord Associates, Jen-Jackie Claim, in the Big Indian Wash area of Utah are presented.

WIN-60

ACID IEACH - RESIN-IN-PULP PILOT PLANT TESTING OF RIO de ORO DYSART SHAFT ORE. A. W. Griffith, M. A. Peters, W. D. Charles and R. L. Shimmin. January 7, 1957. 49 p.

During the period of April 27 to June 8, 1956, Rio de Oro Dysart Shaft Ore from the Ambrosia Lake District, New Mexico, was treated in the Acid Leach - Resin-In-Pulp Pilot Plant at Grand Junction, Colorado. The report contains information on grinding, leaching, sand-slime separation, ion exchange, solvent extraction of H₂SO₄ pregnant eluates, and precipitation. Results show the ore to be amenable to the Resin-In-Pulp process.

WIN-61

TECHNIQUES FOR THE EVALUATION OF AMINES AS URANIUM EXTRACTANTS AND PROPERTIES OF SOME SATISFACTORY AMINES. H. G. Petrow, O. A. Nietzel, J. C. Apidianakis, R. W. Lindstrom and C. F. Lubinger. August 26, 1957. 47 p.

Techniques applicable to the evaluation of amine extractants are described. In addition, data determined for several commercial amine products are presented.

WIN-62

ION EXCHANGE - SPECTROPHOTOMETRIC DETERMINATION OF THORIUM. O. A. Nietzel, B. Wessling and M. A. DeSesa. February 15, 1957. 16 p.

A sensitive method of analysis was needed for the determination of thorium in connection with studies in this laboratory on the production of thorium-free uranium concentrates. Two ion exchange procedures were developed for the separation of thorium prior to spectrophotometric determination with thorin reagent. In the anion exchange procedure, possible cation interferences are removed by adsorption of their chlorö

WIN-62 (continued)

complexes from 9M hydrochloric acid onto Dowex-1 resin. The more specific cation exchange method consists of adsorption of cations from the sample onto Amberlite IR-120 resin, elution of most of the cations with 2M hydrochloric acid, and recovery of the thorium by elution with 3M sulfuric acid. The developed procedures were successfully used to determine thorium in a variety of samples and should find application in the determination of low concentrations of thorium in other complex materials.

WIN-63

IMPROVEMENTS IN THE FLUOR CMETRIC DETERMINATION OF URANIUM. F. A. Centanni and T. J. Morrison, Jr. April 3, 1957. 22 p.

Modifications in the instrumentation and method used in the fluorometric determination of uranium are reported. The elimination of the reference source in the Galvanek-Morrison Fluorimeter has improved the operating stability of the instrument and simplified its operation. Also reported is an automatic fusion burner unit, which minimizes the atmosphere-temperature fluctuations and makes possible better reproducibility and greater accuracy in the uranium determination.

WIN-64

AMENABILITY TESTING OF ADDITIONAL SAMPLES FROM THE AMBROSIA LAKE DISTRICT. R. U. Johnson, H. I. Viklund and E. J. Hammond. May 12, 1958. 25 p.

This report presents the results of laboratory amenability testing of five additional samples of ore from the Ambrosia Lake District in New Mexico. The test work includes acid and carbonate leaching, settling and filtration testing, and solvent extraction of acid leach liquors.

WIN-65

LABORATORY INVESTIGATION OF RIVERTON STOCKPILE ORE. E. S. Porter and H. I. Viklund. March 4, 1957. 23 p.

The results of metallurgical tests of samples of ore from stockpiles one and two at the Riverton, Wyoming ore buying station are reported.

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF U & I ORE. A. W. Griffith, W. A. Millsap and G. Winslow. January 28, 1957. 56 p.

During the period November 8, 1955, through February 12, 1956, U & I ore from the Hecla Mining Company's Fortunate Claim and from the Hidden Splendor Mining Company's Farwest Claim was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. The report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of these ores. A section on mill design considerations is also included. Results show the ores to be amenable to the Alkaline Leach - Filtration process.

WIN-67

ALKALINE IEACH - FILTRATION PILOT PLANT TESTING OF RIO de ORO DYSART SHAFT ORE. R. G. Beverly, W. A. Millsap and G. Winslow. February 15, 1957. 57 p.

During the period of May 11 to July 25, 1956, Rio de Oro Dysart Shaft Ore from the Ambrosia Lake District of New Mexico was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. The report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Both Pachuca and autoclave leaching were employed. Results show the ore to be amenable to the Alkaline Leach -Filtration process.

WIN-68

AMENABILITY TESTING OF HOMESTAKE NORTH ALICE MINE ORE. H. I. Viklund and E. J. Hammond. May 20, 1957. 23 p.

The results of laboratory amenability testing of an ore sample from the Homestake Mining Company, North Alice Mine, in the Big Indian Wash District of Utah, are presented.

PRELIMINARY PILOT PLANT INVESTIGATION OF THE ACID LEACH -CCD - SOLVENT EXTRACTION PROCESS AS APPLIED TO WHITE CANYON ORES. A. W. Griffith, H. E. Gardner and R. L. Shimmin. April 12, 1957. 43 p.

The preliminary operation of the Acid Leach - CCD -Solvent Extraction Pilot Plant at Grand Junction, Colorado, was conducted from November 8, 1956 to January 3, 1957 using White Canyon ores. The report contains information on the grinding, leaching, and liquid-solid separation by continuous countercurrent decantation. Detailed information is presented on the liquid-liquid solvent extraction of the leach liquor using organic solvents containing di-2-ethylhexyl phosphoric acid or triisooctyl amine. Results show White Canyon ores to be amenable to the Acid Leach - CCD - Solvent Extraction process. Using di-2-ethylhexyl phosphoric acid, reagent consumptions were relatively high, whereas with triisooctyl amine excellent recovery of uranium was obtained with moderate reagent requirements.

WIN-70

ACID LEACH RESIN-IN-PULP PILOT PLANT TESTING OF MONTICELLO BLEND ORE. A. W. Griffith, M. A. Peters, W. D. Charles and H. E. Gardner. March 28, 1957. 59 p.

Uranium ore from the Monticello, Utah, stockpile consisting of 40 per cent Stockpile 68, 40 per cent Stockpile 56, and 20 per cent Stockpile 30 was treated in the Acid Leach - Resin-In-Pulp Pilot Plant at Grand Junction, Colorado, from June 15 through August 31, 1956. The name Monticello Blend was given the above mixture. This report presents information on leaching, ion exchange, solvent extraction of pregnant eluate, precipitation, and tailing neutralization tests obtained while treating Monticello Blend. From the pilot plant test, it was concluded that the ore is amenable to the Resin-In-Pulp process.

WIN-71

LABORATORY INVESTIGATION OF SCHWARTZWALDER RALSTON CREEK ORE' E. S. Porter and H. I. Viklund. November 4, 1957. 30 p.

The results of metallurgical tests of samples of ore from the Schwartzwalder Mine, Ralston Creek Area, Colorado, are reported.

PILOT PLANT INVESTIGATION OF THE ACID LEACH - FILTRATION -SOLVENT EXTRACTION PROCESS AS APPLIED TO RIO de ORO DYSART SHAFT ORE. R. G. Beverly, D. O. Skiles and R. L. Shimmin. March 29, 1957. 57 p.

From January 4 to February 18, 1957, operation of the Acid Leach - Filtration - Solvent Extraction Pilot Plant was studied with Rio de Oro Dysart Shaft ore from the Ambrosia Lake area in New Mexico as the ore feed. This report contains information on grinding and leaching of the ore, filtration of the leach residue, solvent extraction of the leach liquor, stripping of the pregnant solvent, and precipitation of yellow cake. The test work was divided into two periods. The first period was conducted with triisooctyl amine as the solvent extractant. High solvent entrainment losses and precipitation of a molybdenum - amine compound in the solvent circuit led to the second period of test work during which Amine 9D-178 was the extractant.

WIN-73

PILOT PLANT STUDIES OF ATMOSPHERIC AND PRESSURE LEACHING OF URANIUM ORES IN ALKALINE SOLUTIONS. R. G. Beverly, W. A. Millsap, and G. Winslow. June 11, 1957. 39 p.

During 1955 and 1956 numerous studies were made in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado, comparing leach results in an autoclave and Pachuca tanks. These studies were made on several different ores including LaSal, Utex, Todilto Limestone, and Rio de Oro Dysart Shaft. The report presents the results of these studies and the effect of several variables such as contact time, temperature, and partial pressure of oxygen a variable which is determined not only by the total pressure of the system and the vapor pressure of water, but also by the rate at which consumed oxygen is replaced. Estimated utility costs for operation of different leaching equipment used are also presented. The report concludes that increasing temperature reduces contact time appreciably, and total air addition can be reduced by use of higher pressures. Leaching under pressure requires less steam and power than at atmospheric pressure.

WIN-74

AMENABILITY TESTING OF LAKEVIEW ORES. D. R. George and R. U. Johnson. August 15, 1957. 38 p.

This report presents the results of laboratory amenability testing of five samples of ore from the Lucky Lass and White King Claims of the Lakeview Mining Company in Lake County, Oregon. The test work includes acid and carbonate leaching, settling and filtration testing,

WIN-74 (Continued)

and ion exchange of acid leach liquors. Rather extensive investigations of the use of solvents to extract the uranium have been made and the results are being presented in a separate report.

WIN-75

PILOT PLANT TESTING OF SOLVENT EXTRACTION OF ACID RIP PREGNANT ELUATES. W. D. Charles, H. E. Gardner, M. A. Peters, and R. L. Shimmin. June 10, 1957. 42 p.

From May 10 to October 29, 1956, sulfuric acid elution was substituted for nitrate elution in the Acid Resin-In-Pulp Pilot Plant. The pregnant eluate was subjected to solvent treatment in a pulse column and in mixer-settlers. The extractant was di-2-ethyl hexyl phosphoric acid. The report contains detailed information on sulfuric acid elution of ion exchange resin, solvent extraction of pregnant eluate, and precipitation of pregnant carbonate solution.

WIN-76

ACID LEACH CCD - COLUMNS PILOT PLANT TESTING OF RIO de ORO DYSART SHAFT ORE. W. A. Millsap and R. L. Shimmin. November 1, 1957. 36 p.

During the period of January 8 to February 18, 1957, Rio de Oro Dysart Shaft ore from the Ambrosia Lake District of New Mexico was treated in the Acid Leach - CCD - Columns Pilot Plant at Grand Junction, Colorado. The report contains detailed information on the liquid - solid separation by continuous countercurrent decantation, ion exchange, and precipitation in connection with the processing of this ore. A section is included on mill design considerations. Results show the ore to be amenable to the Acid Leach - CCD - Ion Exchange Columns process.

WIN-77

THE ALKALINE LEACH - RESIN-IN-PULP PROCESS AS APPLIED TO TODILTO, MESA TOP, AND LA SAL ORES. P. N. Thomas and R. L. Shimmin. September 10, 1957. 106 p.

Test work toward development of the Alkaline Leach Resin-In-Pulp process has been conducted. Todilto Stockpile 53 ore from the Grants, New Mexico area was treated from April 7, to June 18, 1956, Mesa Top ore from the Ambrosia Lake district from June 22 to August 26, 1956, and LaSal ore from December 11 through December 24, 1956. The

WIN-77 (Continued)

report contains data on leaching, reagent recovery, sand-slime separation, ion exchange, and precipitation characteristics of those ores. The data show that the ores reported herein are amenable to the Alkaline Leach-RIP process.

WIN-78

ACID LEACH RESIN-IN-PULP AND CCD SOLVENT EXTRACTION PILOT PLANT TESTING OF LAKEVIEW ORE. W. A. Millsap and R. L. Shimmin. March, 1958. 54 p.

During the period of February 21 to May 30, 1957, Lakeview ore from the Lakeview Mining District of Oregon was treated in the Acid Leach RIP Pilot Plant and the Acid Leach - CCD - Solvent Extraction Pilot Plant at Grand Junction, Colorado. Both Lakeview Oxidized and Reduced Ores from the White King claim were tested. The report contains detailed information on grinding, leaching, sand-slime separation, countercurrent decantation, ion exchange, solvent extraction, and precipitation in connection with the processing of this ore. Results show the ores to be amenable to both processes. However, frequent regeneration of the resin would be required when treating Lakeview Reduced Ore in an Acid Leach RIP process.

WIN-79

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF GLOBE MINING COMPANY ORE. G. R. Pitmon and G. Winslow. October 18, 1957. 37 P.

During the period of May 17 to June 22, 1957, Globe Mining Company ore from the Gas Hills district of Wyoming was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. The report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Pachuca leaching was employed and results show the ore to be amenable to the Alkaline Leach - Filtration process.

WIN-80

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF GLOBE-VITRO BLEND. G. R. Pitmon and G. Winslow. December 12, 1957. 32 p.

During the period of April 11 to May 17, 1957, a blend of Globe Mining Company and Vitro Stockpile ores from the Gas Hills district of Wyoming was treated in the Alkaline Leach - Filtration

WIN-80 (Continued)

Pilot Plant at Grand Junction, Colorado. This report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Pachuca leaching was employed and the circuit liquors contained organic material that was detrimental to clarification and precipitation and the results show that the ore was not amenable to the Alkaline Leach - Filtration process unless a special additive was used.

WIN-81

PILOT PLANT TESTING OF DAKOTA LIGNITES. G. R. Pitmon, M. A. Peters, G. Winslow, H. E. Gardner and R. L. Shimmin. October 18, 1957. 142 p.

The report deals with the pilot plant investigation of recovering uranium from Dakota lignites. Details on FluoSolids roasting, acid leaching, washing and solvent extraction are presented.

WIN-82

ALKALINE LEACH RESIN-IN-PULP PILOT PLANT TESTING OF URANIUM REDUCTION BLEND. H. E. Gardner, M. A. Peters, G. Winslow and R. L. Shimmin. January 15, 1958. 58 p.

During the period August 15 to November 2, 1957, a blend of ores to be processed by the Uranium Reduction Company, Moab, Utah, was treated in the Alkaline Leach - RIP Pilot Plant at Grand Junction, Colorado. The report contains detailed information on grinding, leaching, reagent recovery, sand-slime separation, ion exchange, and precipitation as related to the processing of this ore. Autoclave leaching was employed and results show the ore to be amenable to the Alkaline - RIP process.

WIN-83

ALKALINE LEACH RESIN-IN-PULP PILOT PLANT TESTING OF MONUMENT VALLEY ORE. W. D. Charles and R. L. Shimmin. June 1, 1958. 43 p.

During the period of November 27, 1955 through January 31, 1956, various portions of the Monument Valley ore, Monticello Stockpile 46, were treated in the Alkaline Leach Resin-In-Pulp Pilot Plant at Grand Junction, Colorado, to study ion exchange characteristics with a low uranium to vanadium ratio in the ion exchange feed. The uranium to vanadium concentrations were such that a ratio as low as

WIN-83 (Continued)

1.5:1 was attained with no detrimental effect on the ion exchange characteristics. The report contains detailed information on grinding, leaching, sand-slime separation, ion exchange, and precipitation as related to the processing of this ore.

WIN-84

ALKALINE LEACH - CCD - COLUMN ION EXCHANGE PILOT PLANT TESTING OF AMBROSIA LAKE ORES. H. L. Ford, J. R. Ruark, and R. L. Shimmin. June 16, 1958. 54 p.

Test work devoted to development of the Alkaline Leach -CCD - Column Ion Exchange Process was performed at the Grand Junction Pilot Plant from November 4, 1957 to February 2, 1958. This report presents data on leaching, reagent recovery, countercurrent decantation, column ion exchange, and precipitation characteristics of the Rio de Oro Dysart Shaft and Holly Minerals Company ores from the Grants, New Mexico area.

WIN-85

THE USE OF POWDERED SPECIMENS FOR STUDYING THE KINETICS OF DISSOLUTION. W. E. Schortmann and M. A. DeSesa. November 18, 1957. 34 p.

Because of the difficulty involved in preparing massive specimens, the feasibility of using powdered material in kinetic studies of liquid-solid systems was investigated. It was shown that, contrary to published opinion, the powder method for studying the dissolution of solids is as valid as the massive specimen technique. Consequently, the advantages of using a fine powder warrant consideration of its use in studying the kinetics of these heterogeneous systems. The main advantages are ease of sample acquisition and preparation and simplicity of experimental procedure.

WIN-86

OXIDANTS IN CARBONATE LEACHING OF URANIFEROUS ORES. P. J. Magno and M. A. DeSesa. August 23, 1957. 44 p.

In order to obtain data on the comparative effectiveness of oxidants for uranium in alkaline carbonate solutions, a variety of reagents were used under identical conditions for the dissolution of uranium dioxide in 0.5M sodium carbonate and 0.5M sodium bicarbonate. Those oxidants which appeared most promising were evaluated further in

WIN-86 (Continued)

leaching studies on E. L. Cord and La Sal ore samples. As a result of these tests, the cupric ammonia complex ion was determined to be the most economical oxidant for the carbonate leaching of uraniferous ores. Further evaluation of the copper-ammonia reagent on other ores, which were known to require an oxidant during carbonate leaching, indicated that this reagent is effective on all ores tested.

WIN-87

LABORATORY INVESTIGATION OF MOONLIGHT CLAIM ORE. E. S. Porter, H. I. Viklund and E. J. Hammond. March 3, 1958. 19 p.

The results of laboratory metallurgical investigations of a sample of ore from the Moonlight Claim of the Industrial Minerals Corporation are reported. The amenability of the sample to acid and carbonate leaching techniques and methods of recovery of uranium from acid solution were studied.

WIN-88

LABORATORY STUDIES IN CARBONATE ION EXCHANGE FOR URANIUM RECOVERY. E. T. Hollis. May 1, 1958. 52 p.

The results of laboratory studies on sodium carbonate ion exchange are shown. The effect of salt concentration, uranium concentration, and possible interference with ion exchange from vanadium, molybdenum, sulfate and chloride are discussed. Various elution systems and the effect of residual uranium are described. A short discussion of ammonium carbonate ion exchange is also presented.

WIN-89

KINETICS OF THE DISSOLUTION OF URANIUM DIOXIDE IN CARBONATE-BICARBONATE SOLUTIONS. W. E. Schortmann and M. A. DeSesa. March 12, 1958. 62 p.

The kinetics of the dissolution of uranium dioxide in sodium carbonate-sodium bicarbonate solutions were determined. The study was undertaken in order to obtain fundamental information about the commercial carbonate process for leaching uranium from its ores. A rate equation incorporating the effects of surface area, oxygen partial pressure, temperature, and reagent concentrations was empirically developed. A mechanism consisting essentially of two consecutive reactions at steady state is proposed. These reactions are the oxidation of U(IV) to U(VI) and the subsequent formation of the uranyl dicarbonate complex ion. Depending on the conditions,

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WIN-89 (Continued)

either or both of these reactions can determine the over-all rate. The conversion of uranyl dicarbonate to the uranyl tricarbonate complex ion is postulated to be very rapid. In the suggested mechanism, the rate-determining phase of the oxidation is the dissociation of adsorbed molecular oxygen, and both the carbonate and bicarbonate ions play equivalent roles in the formation of the uranyl dicarbonate. As indicated by their high activation energies of about 13 and 14 kcal per mole uranium, both reactions are chemical rather than diffusional processes. A mathematical examination of the proposed mechanism produced a rate equation consistent with the experimental information. The credibility of the mechanism was thereby strengthened.

WIN-90

PREPARATION OF DENSE, METAL-GRADE UF4 FROM ORES AND CONCENTRATES. H. G. Petrow, R. J. Allen and P. J. Magno. May 15, 1958. 64 p.

A process for the preparation of dense, metalgrade UF4 from ores and concentrates is described.

WIN-91

AMENABILITY TESTING OF LABAJADA ORE. R. U. Johnson. April 17, 1958. 15 p.

Data are presented on the results of acid and carbonate leaching studies on samples of ore from the LaBajada Mine of the Lone Star Mining Company, Santa Fe County, New Mexico.

Not for general distribution.

WIN-93

Unused number.

WIN-94

Unused number.

WIN-95

THE DEHYDRATION OF GREEN SALT, UF4. A. Whitman and R. Lindstrom. May 1, 1959. 40 p.

Several methods have been investigated for the dehydration of green salt produced by precipitation from aqueous solution. As a result of this investigation a procedure was devised in which metal-grade salt was produced by dehydration in a tube furnace at 400-500°C. Using this method, no special furnace atmosphere is required. An air flush is used to provide the proper oxidation after most of the moisture is removed from the salt. The method was successfully used to dehydrate almost 200 pounds of green salt.

WIN-96

AMENABILITY TESTING OF ST. ANTHONY ORE. H. I. Viklund and E. J. Hammond. May 9, 1958. 13 p.

The results of laboratory amenability testing of an ore sample from the St. Anthony Uranium Corporation, in Valencia County, New Mexico, are presented.

WIN-97

AMENABILITY TESTING OF ORE SAMPLES FROM THE GAS HILLS DISTRICT OF WYOMING. H. I. Viklund, E. J. Hammond and R. U. Johnson. July 10, 1958. 22 p.

Data are presented to show that various ores from the Gas Hills area of Wyoming are amenable to leaching with acid or . carbonate solutions. The effect of soluble organic matter in the ores is considered.

LABORATORY INVESTIGATION OF MALLINCKRODT BOMB LINER SLAG. E. S. Porter. June 13, 1958. 49 p.

Data are given for leaching Mallinckrodt magnesium fluoride and dolomite slag in acid and alkaline systems. Recovery of dissolved values is considered using direct precipitation, ion exchange, or solvent extraction.

WIN-99

CHEMICAL STREAM POLLUTION FROM URANIUM MILLS. A. Whitman and E. S. Porter. June 13, 1958. 43 p.

A study of chemical pollution of water supplies caused by tailings discharge from domestic uranium mills is presented. State water specifications are surveyed, the extent and nature of pollution are evaluated, and remedies are suggested.

WIN-100

CONTINUOUS COUNTERCURRENT SOLVENT LEACHING. P. Galvanek, Jr. July 16, 1958. 43 p.

Continuous countercurrent non-aqueous leaching techniques are described for the recovery of uranium directly from a variety of conditioned ores. No preliminary gangue separation is involved. Product grades exceeding 99 per cent U308 are achieved. Several methods for uranium solubilization and ore conditioning by the acid-cure technique are described. Both primary and secondary ores were successfully treated. A bibliography of literature pertaining to the solvent leaching technique from its inception is included.

WIN-101

INTERIM REPORT ON INVESTIGATIONS INTO THE PROBLEM OF RADIO-ACTIVE POLLUTION OF URANIUM MILL EFFLUENTS. M. A. DeSesa. December 15, 1958. 61 p.

A review of the laboratory investigations to date into the problem of radioactive pollution of uranium mill effluents is presented. The scope of the problem is defined, preliminary survey data are outlined, and detailed investigations into means of alleviating the problem are presented.

A CONTINUOUS COUNTERCURRENT RESIN-IN-PULP PROCESS. J. B. Breymann, E. T. Hollis and J. T. Lynch. July 18, 1958. 32 p.

Data are reported for a continuous 1375 pound per day pilot plant run of a countercurrent resin-in-pulp process using air agitated tanks and conventional vibrating screens in the adsorption circuit and continuous countercurrent column elution in the recovery circuit. Some data are given to indicate the physical stability of various anion exchange resins in use in this type of process.

WIN-103

CONTROL OF ORGANICS IN CARBONATE LEACHING CIRCUITS. D. R. George and J. T. Lynch. July 25, 1958. 35 p.

The results of experiments with methods of controlling soluble organics in the carbonate leaching of uranium ores are described. The methods studied include the uses of adsorbents, chemical oxidants, precipitants, electrolytic oxidation, and air oxidation by high-temperature autoclaving.

WIN-104

SOME EXPERIMENTS WITH AERATION AND AGITATION OF CARBONATE LEACHING SLURRIES. G. W. Clevenger and R. A. Eisenhauer. June 23, 1958. 28 p.

Data are presented on the effect of various amounts and methods of aeration on uranium leaching extraction and power requirements of mechanical agitators. The effect of tank depth on air oxidation is considered.

WIN-105

LABORATORY INVESTIGATION OF SINGLE-STAGE AND CONTINUOUS COUNTERCURRENT ION EXCHANGE METHODS. E. T. Hollis and R. J. Woody. July 1, 1958. 36 p.

The report describes the initial stages of the development of methods of continuous ion exchange processes including (1) a combination of two stage leaching and recovery of uranium in a single stage resin-in-pulp contact, (2) elution of uranium WIN-105 (Continued)

in a continuous countercurrent column and (3) exhaustion of uranium from leach liquor in the continuous countercurrent column. Test results are also presented on the effect of variables on resin loading and uranium recovery by single stage contact for solution to resin ratios in the range of 25-100 to one.

WIN-106

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF MONTI-CELLO BLEND OF HIGH LIME ORES. H. E. Dixon and G. Winslow. March 14, 1958. 32 p.

During the period of January 2 to January 23, 1958, a blend of LaSal, Standard, and Jen ores from the Monticello stockpiles was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. This report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Autoclave leaching and continuous NaOH precipitation were employed. The results show the ore to be amenable to the Alkaline Leach - Filtration process.

WIN-107

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF HOMESTAKE ORE - SECTION 32. H. E. Dixon and G. Winslow. June 9, 1958. 33 p.

During the period of January 23 to February 12, 1958, Homestake Ore (Section 32) from the Ambrosia Lake District of New Mexico was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. This report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Autoclave leaching and continuous yellow cake precipitation were employed. The circuit liquors contained organic material that was detrimental to clarification and precipitation and the results show that the ore was amenable to the Alkaline Leach - Filtration process only if a special additive was used.

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF HOLLY MINERALS COMPANY ORE. H. E. Dixon and G. Winslow. June 9, 1958. 43 p.

During the period of February 15 through April 1, 1958, Holly Minerals Company ore from the Ambrosia Lake District of New Mexico was treated in the Alkaline Leach - Filtration Pilot Plant at Grand Junction, Colorado. The report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Both autoclave and Pachuca leaching were employed. Results show the ore to be amenable to the Alkaline Leach - Filtration process.

WIN-109

ACID LEACH-CCD-SOLVENT EXTRACTION PILOT PLANT TESTING OF HOLLY MINERALS COMPANY ORE. M. A. Peters and R. L. Shimmin. June 20, 1958. 66 p.

During the period of February 10 to May 8, 1958, Holly Blend ore from the Holly Minerals Company of the Ambrosia Lake District in New Mexico was treated in the Acid Leach - Countercurrent Decantation - Solvent Extraction Pilot Plant at Grand Junction, Colorado. This report contains detailed information on leaching, countercurrent decantation, clarification, and solvent extraction as applied in the processing of this ore. Results show the ore to be amenable to the Acid Leach - Countercurrent Decantation - Solvent Extraction process.

WIN-110

ALKALINE LEACH - FILTRATION PILOT PLANT TESTING OF PHILLIPS PETROLEUM COMPANY ORE. H. E. Dixon and G. Winslow. July 1, 1958. 54 p.

During the period of April 3 through May 28, 1958, Phillips Petroleum Company ore (Section 28) from the Ambrosia Lake District of New Mexico was treated in the Alkaline Leach -Filtration Pilot Plant at Grand Junction, Colorado. This report contains detailed information on grinding, leaching, filtration, and precipitation in connection with the processing of this ore. Both pressurized and atmospheric Pachuca leaching followed by filtration and continuous yellow cake precipitation were employed. The results show that the ore was amenable to the Alkaline Leach -Filtration process.

WIN-115 - 67 -

WIN-111

SECOND INTERIM REPORT ON INVESTIGATIONS INTO THE PROBLEM OF RADIO-ACTIVE POLLUTION OF URANIUM MILL EFFLUENTS. M. A. DeSesa. April 1, 1959. 75 p.

A review of the laboratory and plant investigations for the period December 16, 1958 to March 31, 1959 into the problem of radioactive pollution of uranium mill effluents is presented.

WIN-112

THIRD INTERIM REPORT ON INVESTIGATIONS INTO THE PROBLEM OF RADIO-ACTIVE POLLUTION OF URANIUM MILL EFFLUENTS. R. G. Beverly September 30, 1959. 112 p.

A review of the laboratory and plant investigations conducted between April 1, 1959 and September 1, 1959 into the problem of radioactive pollution from uranium mill effluents is presented, methods of decontamination for radium and thorium, treatment studies on acid and alkaline mill tailings, U-Ra-Th equilibrium ratios in ores, and Ra-Th balances in uranium mills are discussed.

WIN-113

RADIUM BALANCE IN THE MONTICELLO ACID R.I.P. URANIUM MILL. A. Whitman and R. G. Beverly. December 30, 1958. 48 p.

A study of radium distribution through the Monticello Acid Resin-in-Pulp plant is presented. Emphasis is placed on the flow of radium through the process in an effort to determine the effect of the uranium treatment process on the dissolution and the ultimate disposition of radium.

WIN-114

SURVEY AND PREVENTION TECHNIQUES FOR CONTROL OF RADIOACTIVITY HAZARDS AT THE MONTICELLO URANIUM MILL. R. G. Beverly. December 15, 1958. 65 p.

This report describes the techniques used in sampling, analyzing, and evaluating results for determining hazards from external radiation, airborne radioactive material, radioactive
WIN-114 (Cont'd)

contaminants in mill effluents, and urinary uranium, as applied to the Monticello, Utah, uranium mill. Corrective measures used by National Lead Company, Inc., at the Monticello Mill are described along with the results from later surveys which showed large reductions in the potential radiation hazards. Details are given of the methods used to determine personnel exposures to radioactive and silicosis-producing dusts, potential external radiation hazards and in assaying mill effluents for uranium and radium, assaying urine samples for uranium, as well as the standard operating procedures issued at Monticello to employees for preventing and/or controlling personnel exposures.

TOPICAL REPORTS

AMERICAN CYANAMID COMPANY (From ACCO-67)

Number	Authors	Title	Date of <u>Issue</u>
ACCO-1		Progress Report	3/51
ACCO-2	Woody	Possible Substitutes for Glue in South African Ore Treatment	5/51
ACCO-3	×	Progress Report	5/51
ACCO-4		Progress Report	8/51
ACCO-5	Abrams, Woody	Leaching and Precipitation Tests on Grants Ores	9/51
ACCO-6		Progress Report	11/51
ACCO-7	Brunner, George, Rubino	Preliminary Report on Recovery of Uranium from Low Grade Belgian Congo Ores	10/51
ACCO-8	Abrams	Ion-Exchange Studies on Carbonate Leach Liquors from Grants, New Mexico Ores	10/51
ACCO-9	George, Kennedy, Howland, Rubino	Preliminary Report on Recovery of Uranium from High Carbonate Belgian Congo Uranium Ores	10/51
ACCO-10	Breymann	Application of Heavy Media Separation, Flotation and Carbonate Leaching to Congo Ores	10/51
ACCO-11	Kennedy Howland	Recovery of Uranium from Congo Leach Liquors with Ion Exchange Resins	10/51
ACCO-12	Pannell, Michal, Thorpe, Lower, Bloecher	Elution of Uranium from Anion Exchange Resins by Pregnant Rand Solutions	4/53

ACCO REPORTS (Continued)

Number	Authors	Title	Date of Issue
ACCO-13	Bloecher	Filtration, Drying and Calcining Tests on Rand Precipitates	11/51
ACCO-14	Bloecher	Calcining-Amenability Testing of Rand Precipitates	11/51
ACCO-15		Progress Report	12/51
ACCO-16	Bloecher	Uranium Recovery from Thomas Range, Utah Fluorspar	1/52
ACCO-17		Progress Report	1/52
ACCO-18	R. Hollis, Breymann, Lynch	Preliminary Leaching Investiga- tion of Ores from Radium Hill, South Australia	6/52
ACCO-19	Clevenger	Experimental Work for the Develop- ment of a Process to Treat Luka- chukai Ores	6/52
ACCO-20		Progress Report	4/52
ACCO-21	R. Hollis, Lynch	Preliminary Leach Investigation of Babrosco and Afrikander Lease Residues	5/52
ACCO-22	George	Recovery of Uranium by Ion Exchange or by Uranous Phosphate Precipita- tion from Sulfuric Acid Leach Solu- tions Produced from Australian Davidite Ore Concentrates	6/52
ACCO-23	Owens	Recovery of Manganese Dioxide from Rand Barren Solutions	3/52
ACCO-24	George	Recovery of Uranium from High Grade Australian Rum Jungle Uranium Ore	8/52
ACCO-25	Clevenger	A Regenerative Electrolytic Process for Recovering Uranium from Ores	8/52
ACC0-26	Abrams, Kaufman	Preliminary Studies of the Adsorp- tion of Uranium in a Resin-in-Pulp System	7/53

ACCO REPORTS (Continued)

Number	Authors	Title	Issue
ACCO-27	Bloecher	Uranium Recovery from a Temple Mountain District Ore Sample	10/52
ACCO-28	Breymann, George	Tests on Samples of Copper- Uranium Ore from Rum Jungle Deposit, Northern Territory, Australia	1/53
ACCO-29	Clevenger	The Application of the Electrolytic Uranium Recovery Process to Lime- stone Ore from Grants, New Mexico	9/53
ACCO-30	Abrams, Moulton, Viklund	Preliminary Leaching Tests for the Extraction of Uranium from Various Monticello Stockpile Ores	3/53
ACCO-31	Kennedy	Examination of Poisoned Ion Exchange Resins from the Western Reefs Pilot Plant	2/53
ACCO-32	Brown	Metallurgical Investigation of Various Grants, New Mexico, Lime- stone Ores	5/53
ACCO-33	Jones, Viklund	Additional Extraction and Ion Ex- change Studies of Temple Mountain District Ores	7/54
ACCO-34	Viklund, Kennedy	Removal of Chloride from Congo Precipitates	11/53
ACCO-35	Schiff, Lower, E. Hollis	The Effect of Molybdenum on Uranium Adsorption and Subsequent Cyclic Column Testing of Leach Liquor	3/54
ACCO-36	Brown	Preliminary Investigation of Carbon- ate Leaching	10/53
ACCO-37	Pickwick	Ion Exchange Studies on Acid Leach Liquors from Durango Residues	1/54

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ACCO REPORTS (Continued)

Number	Authors	Title	Date of Issue
ACCO-38	Breymann	Progress Report on the Flotation of Uranium Bearing Minerals from Lake Athabaska Ore, Sample 43-1	10/53
ACCO-39	Breymann, Richardson	A Copper-Uranium Ore from Rum Jungle, Northern Territory, Australia	11/53
ACCO-40	Clevenger	A Pilot Plant Test of the Electroly- tic Uranium Recovery Process	6/54
ACCO-41	Stanley, George, Thomas, Eisenhauer, Lynch, Richardson	Utex Leaching, Thickening and Fil- tration Tests	3/54
ACCO-42	R. Hollis, Abrams, McArthur, Izzo	The Development of a Resin-in-Pulp Process and its applications to ores of the White Canyon Area of Utah	6/54
ACCO-43	E. Hollis, Pickwick, Kazanjian, Larson, Howland, Porter	Ion Exchange Tests on Liquors and Pulps Produced from Utex Ores	7/54
ACCO-44	Schiff, Lower	Investigations of Ion Exchange Methods for Recovery of Uranium from Liquors Produced by Acid Leaching of Gunnar Ore	6/54
ACCO-45	E. Hollis, McLean	Precipitation of Red Cake from Low Vanadium Acid Sulfate Leach Liquors	10/54
ACCO-46	Schiff, Viklund	Recovery of Uranium from Vitro Leach Liquor by Ion Exchange, Part II, Cyclic Column Tests Comparing IRA-400 and XE-75 Resins and Cyclic Testing of a Resin-in-Pulp System	5/54

ACCO REPORTS (Continued)

Number	Authors	Title	Date of Issue
ACCO-47	Galvanek, Morrison	A New Fluorimeter for the Deter- mination of Uranium	5/54
ACCO-48	Frank	Summary of Carbonate Leaching of Uranium Ores	6/54
ACCO-49	Frank	The Chemistry of Vanadium-A Summary of Non-Froject Literature through November, 1952	6/54
ACCO-50	Thorpe, Schiff, Cole, Pickwick, Lynch	Ion Exchange of Grants Acid Leach Liquors	7/54
ACCO-51	Stanley	Vanadium Salt Roasting Studies	7/54
ACCO-52	Stanley, Eisenhauer, Richardson	Two-Stage Leaching Tests on Utex Ore	7/54
ACCO-53	Abrams, Izzo	The Recovery of Vanadium by Ion Exchange	7/54
ACCO-54	DeSesa, Nietzel	Spectrophotometric Determination of Uranium with Thiocyanate	7/54
ACCO-55	Zingaro	Studies on Direct Extraction of Uranium from Synthetic Ores by Non-Aqueous Systems	7/54
ACCO-56	Moulton	Utex Ore Stockpiled at Monticello	7/54
ACCO-57	R. Hollis, Abrams, McArthur, Izzo, Wilson	Pilot Plant Tests on Anaconda Ore from Grants District, Grants, New Mexico	7/54
ACCO-58	Moulton	Field Work Performed at Monticello, Utah, Including Stockpile Amenabilit and Ion Exchange	7/54 y

ACCO REPORTS (Continued)

			Date of
Number	Authors	Title	Issue
ACCO-59	Kazanjian	Systematic Elution Studies, Part I, The Effect of Sul- fate Accumulation on the Elution of Uranium from Strong Base Ion Exchange Resins with Chloride	7/54
ACCO-60	Tooney, Kaufman	The Relationship Between Oxidation and Reduction Potential and Valence State of Iron, Vanadium and Uranium in Sulfuric Acid Leach Liquors	7/54
ACCO-61	0'Connor	Ion Exchange Studies, Part I, Equilibrium Constants, Part II, Nature of Uranium Adsorption	7/54
ACCO-62	O'Rourke, Ladner	Investigation of the Poisoning of West Rand Anion Exchange Resins	7/54
ACCO-63	McLean, E. Hollis, Eisenhauer, Shepherdson, Cole	Development of an Ion Exchange Process for the Recovery of Vanadium	7/54
ACCO-64	McLean	Process Development Studies for Lukachukai Ores	4/55
ACCO-65	Charles, Thorpe, Lower, Kaufman, Schiff, Abrams, Porter, Viklund, Howland	The Development of Fixed Screen Resin-in-Pulp Devices	8/54
ACC0-66	Ladner, Lower	Laboratory Scale Abrasive Tests on Ion Exchange Resins	7/54
ACCO-67	Allen	A Summary of Research and Develop- ment Work on Low Grade Uranium Ores	5/55
ACCO-68	Kaufman, Lower	A Summary Report on the Ion Exchang Process for the Recovery of Uranium	e 7/54

TOPICAL REPORTS

MIT MINERAL ENGINEERING LABORATORY (From MITG-270)

Number	Authors	Title	Date of Issue
MITG-PR1	Blake	Flotation Test Work	1/45
MITG-PR2	Blake	Flotation Test Work	2/45
MITG-PR3	Blake	Leaching Tests - 803 Ores and Minerals	4/45
MITG-PR4	Blake, Bowdish	Flowing Film Concentration - Deslimed Ore	5/45
MITG-PR5	Blake	Flotation Test Work (R-10)	5/45
MITG-M1	Melum	Report on Heavy Liquid Separa- tions	3/45
MITG-M2	Gaudin	Mineralogy Report on R-10 Ore	3/45
MITG-M3	Mitchell	Fluorescent Microscopy	4/45
MITG-M4	Schühmann	Treatment of Ore R-10	4/45
MITG-M5	Schuhmann	Inspection Trip - Scrubbing and Washing Equipment	7/45
MITG-M6	Dundon	Use of Centrifugal Apparatus for Desliming and Acid and Alkali Leaching of R-10 Ore at Room Temperature	7/45
MITG-M7	Gaudin	Report of Sample SS94D	10/45
MITG-M8	Schuhmann	Inspection Trip of Leaching Plants	10/45
MITG-M9	Gaudin	Report of Sample SS95E	10/45
MITG-M10	Gaudin	Review of Progress Investiga- tion of African Ores	12/45
MITG-M11	Gaudin	Status of Proposed Treatment Process and Treatment Plant for African Ores	1/46

WIN-115 - 76 -

MIT REPORTS (Continued)

Number	Authors	Title	Date of Issue
MITG-M12	Mitchell	Mineralogy of Sample SS91A	1/46
MITG-ML3	Mitchell	Mineralogy of Ore SS92B	3/46
MITG-M14	Gaudin	Mineralogy of SS97G	7/46
MITG-M15	Mitchell	Mineralogy of Ore SS930	8/4 6
MITG-M16	Mitchell	Mineralogy of Ore SS96F	9/46
MITG-M17	Gaudin, Schuhmann	Investigation of African Ores (Final Report)	10/46
MITG-M18	Gaudin, Tyler	Concerning a National Policy for the Development of Domestic Resources of Fissionable Elements	11/46
MITG-E1	Blake, Bowdish	Ore 89-E - Preliminary Sink- Float Tests	5/45
MITG-E2	Blake, Bowdish, Schuhmann	Concentration Tests on Ore Sample 89-E	7/45
MITG-E3	Bowdish	Preliminary Blunging and Leaching Tests on Ores, A, B, C, D, and F	9/45
MITG-E4	Blake, Gaudin	Gravity Concentration Tests on A, B, C, D, and F	10/45
MITG-E5	Schuhmann, Bowdish, Dundon, Mitchell	Blunging and Sizing Tests	1/46
MITG-E6	Brandenberger	Leaching Experiments on African Ores	3/46
MITG-E7	Dundon, Schuhmann	Precipitation of Leach Liquors and Dewatering of the Precipitate	6/46
MITG-E8	Schuhmann, Brandenberger, Bowdish	Agitation Leaching with Sulfuric Acid-Ferric Sulfate Solution	5/46

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Number	Authors	Title	Date of Issue
MITG-E9	Gaudin	Mineralogical Characteristics and Leaching Behavior of Meta- torbernite of Certain of its Dehydration Products	6/46
MITG-E10	Bowdish	Settling of Ores and Leach Residues	6/46
MITG-Ell	Dundon	Precipitation of Leach Liquors and Dewatering of the Precipitate	7/46
MITG-E12	Bowdish	A preliminary Study of the Extraction of Cobalt from 308 Leach Residue	7/46
MITG-E13	Kneppel	Extraction of Cobalt from African Ores	9/46
MITG-E14	Schiff, Greenewald	Treatment of the Double-Letter Samples of African Ores by Direct Leaching and by Leaching after Removal of Carbonates by Flotation	10/46
MITG-S1	Tyler	Proposed Thorium Program	8/47
MITG-S2	Tyler	Proposed Beryllium Ore Program	8/47
MITG-S3	Tyler	Notes on Source Materials for Atomic Energy	8/47
MITG-S4	-	Minutes of Conference - July 21, 1948	7/48
MITG-S5	Michal	The Oxidation States of Uranium	6/47
MITG-S6	Macdonald	Estimated Cost of Producing Uranium from Rand Ores	4/49
MITG-S7	-	Minutes of Conference August 2 and August 3, 1949	8/49
MITG-S8	Macdonald	Estimated Cost of Producing Uranium from Rand Ores	9/49

Number	Authors	Title	Date of Issue
MITG-S9	Gaudin, Dasher, Pannell, Freyberger	Use of an Induced Nuclear Reac- tion for the Concentration of Beryl	9/49
MITG-S10	Gaudin, Galvanek, Dasher, Kaufman	Leaching of Nitrated Materials with Organic Solvents	9/49
MITG-S11	Gaudin, Dasher, Clevenger	Process for Uranium Recovery from Phosphoric Acid by Re- duction followed by Ammonia Precipitation	9/49
MITG-S12	Macdonald	Trip to the Union of South Africa 11/3 - 12/6/49	12/49
MITG-S13	Kaufman	Memorandum on Patent Actions	12/49
MITG-S14a	Compiled by Kaufman	Research Problems	4/50
MITG-A1	Gaudin	Report on Work Done on Samples Left with us by Dr. Bain	4/46
MITG-A2	Gaudin	Recovery Time in Counter Analyses	5/46
MITG-A3	Gaudin	Preliminary Size, Gravity and Magnetic Fractionations of Ores 396-1 and 396-2	6/46
MITG-A4	Rodden, Chorney, Pannell	Report on Head Analyses for 396-1 and 396-2 Ore by Chemical and Counter Methods	6/46
MITG-A5	Brown	Flotation Testing on Ores Number 396-1 and 396-2	6/46
MITG-A6	Dasher	Probable Errors in Results of Metallurgical Tests of Ore 396-2 Due to Segregation	8/ 46

Number	Authors	Title	Date of Issue
MITG-A7	Brown	Additional Flotation Test Data on Initial Samples of Ores 396- l and 396-2	8/4 6
MITG-A8	Brown	Flotation Tests on Initial Sam- ples of Ores, Number 396-1 and 396-2 after Desliming	8/ 46
MITG-A9	Brown, Dasher, Tyler	Summary of Tests on Initial Samples of Ores 396-1 and 396-2	8/46
MITG-A10	Dasher	Preliminary Flotation Tests on the Large Sample of 396-2	8/46
MITG-All	Chayes	Mineralogy and Fractionation Tests of Main Sample of Ore 396-2	9/46
MITG-A12	Macdonald, Dasher	Further Flotation Tests on 396-2	10/46
MITG-A13	Brunner, Kneppel, Macdonald	Direct Cyanidation of Ore 396-2	10/46
MITG-A14	Dasher, Brown, Macdonald	Further Flotation Testing on 396-2	11/46
MITG-A15	Chayes, Tyler	Mineralogy and Fractionation Tests on Ore 396-1	11/46
MITG-A16	Dasher, Macdonald	Flotation of Cyanided Pulps from Ore 396-2	1/47
MITG-A17	Dasher, Brown, Macdonald	Progress in Flotation Testing of Ore 396-2	1/47
MITG-A18	Dasher, Brown, Macdonald	Miscellaneous Flotation Tests on Ore 396-2	1/47
MITG-A19	Dasher, Brown	Preliminary Report on Testing of Ore 396-1	2/47

WIN-115 - 80 -

MIT REPORTS (Continued)

4

<u>Number</u>	Authors	Title	Date of <u>Issue</u>
MITG-A20	Dasher, Schiff	Ferric Sulphate-Sulphuric Acid Leaching Process Tests on Ore 396-2	1/47
MITG-A21	Dasher, Brunner	Recovery of Gold from Ore 396-2	4/47
MITG-A22	Dasher, Brown, Macdonald	Further Flotation Testing of Ore 396-2	4/47
MITG-A23	Chayes	Mineralogy and Fractionation Tests of Ore 396-5	4/47
MITG-A24	Dasher, Brown, Brunner, Macdonald	Preliminary Testing on Ore 396-5	3/47
MITG-A25	Dasher, Kneppel	Modified Leaching for 396 Ores with Cyclic Recovery of Iron	6/47
MITG-A26	Schiff, Dasher	Miscellaneous Leaching Tests on 396-2 Ore	7/47
MITG-A27	Dasher, Macdonald, Brown, Brunner, Schiff	Further Testing on Ore 396-5	9/47
MITG-A28	Pannell	Radioassay Techniques for Low- Grade U Ores and Mineral Dressing Products	5/47
MITG-A29	Pannell, Rubino, Warren	Radiometric Research	8/47
MITG-A30	Murray	Flotation of Uraninite from Other Minerals	5/47
MITG-A31	Sollenberger	The Design of a Combination- Process Mill	5/47

Number	Authors	Title	Date of Issue	
MITG-A32	Kaufman	Investitgations of Wet Chemical Methods for Analyses for Ura- nium - Special References to Low-Grade Ores	10/47	
MITG-A33	Kaufman, Pannell	Disruption of Radioactive Equi- librium as a Result of Flotation Testing on 396-Ores	12/47	
MITG-A34	D as her, Schiff	Precipitation of Simple Leach Solutions from 396-2 Ore and Thickening the Precipitate	10/47	
MITG-A35	Michal	Electrolytic Precipitation of Uranium from Aqueous Solution	11/47	
MITG-A36	Macdonald, Dasher	Cyclic and Countercurrent Leaching of 396-5 Ore	12/47	
MITG-A37	Dasher	Miscellaneous Tests on Ores 396-2 and 396-5	3/48	
MITG-A38	Brunner	Differential Precipitation of Uranium from Iron by Neutral- ization	6/48	
MITG-A39	Pannell	Preliminary Experiments in Gamma- Counting Flotation Pulps	1/49	
MITG-A40	Dasher, Brown, George, Brunner, Schiff	Tests on Vein Sample 396-3	10/48	
MITG-A41	Dasher, Brown, George, Brunner, Schiff	Tests on Vein Sample 396-4	10/48	
MITG_A42	Macdonald, Brunner, Schiff	Single-Stage, Non-cyclic Leach- ing of 396 Ore	4/48	
MITG-A43	Brunner	Preliminary Experiments on the Use of SO ₂ and Air for Production of Leaching Reagents	6/48	

Number	Authors	Title	Date of Issue
MITG-A44	Bailey	Precipitation of Uranium by Inorganic Acids of Groups V & VI	3/48
MITG-A45	Kaufman, Perkins	The Spectrographic Determina- tion of Uranium in Ores and Ore Products	8/48
MITG-A46	Dasher, Brunner, Brown	Complete Process Tests on Ore 396-5	7/48
MITG-A47	Kaufman, Brunner	Check-Assaying Studies of Gold and Uranium in Products of the Rand Mines	12/48
MITG-A48	Sollenberger, Dasher	Countercurrent Leaching of 396-5 Ore with SO ₂ and Air	4/48
MITG-A49	Murray, Dasher	Carbonate Treatment of 803 Precipitates	6/48
MITG-A50	Brunner, Jackson, Porter	Use of Packed Towers for the SO ₂ - Air Process	9/48
MITG-A51	Michal	The Leaching of Uranium from Insoluble Hydroxides by a Car- bonate Treatment	9/48
MITG-A52	Bailey	Precipitation of Uranium by Organic Compounds	12/48
MITG-A53	Michal	The Recovery of Uranium from Low-Grade Leach Liquors by Selective Precipitation	11/48
MITG-A54	Porter	Cyclic Leaching Tests on 396-53 Cyanided Residue	2/49
MITG-A55	Brown	Non-cyclic Leaching of Refrac- tory Rand Ores	1/49

4

Number	Authors	Title	Date of Issue
MITG-A56	Macdonald	An Investigation of Recovery of Uranium from Rand Gold Ores from April 1946 to July 1948	9/48
MITG-A57	Freyberger, Rubino	Radioassay of Leach Solutions and Residues	2/49
MITG-A58	George	Fractionation Studies of Re- fractory Samples from Bly- vooruitzicht	4/49
MITG-A59	Dasher, Schiff	Miscellaneous Tests on Pre- cipitation of Rand Leach Liquors with Alkali	11/49
MITG-A60	Kennedy, Kaufman	A Microvolumetric Method for the Determination of Small Quantities of Uranium	5/49
MITG-A61	Oberg	Continuous Leaching Test I	2/49
MITG-A62	Bailey	Phosphate Precipitation of Uranium from Rand Ore Leach Solutions and Retreatment of the Phosphate Precipitates	6/49
MITG-A63	Pannell, Rubino, Freyberger, Haney	Radioactivity Measurements at Continuous Countercurrent Leaching Test	3/49
MITG-A64	Schiff	Experiments on Rand Leach Liquors with Cation-Exchange Resins	8/49
MITG-A65	Koskela, Kaufman	The Fluorimetric Determination of Uranium, Part I	5/49 -
MITG-A67	Kaufman, Galvanek	Modifications in the Peroxide- Colorimetric Method for Uranium Developed at the MIT Mineral Engineering Laboratory	7/50

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			Date of
<u>Number</u>	Authors	Title	Issue
MITG-A68	Oberg	Continuous Leaching Test II	5/49
MITG-A69	George	Mineral Fractionation and Leaching Tests on Portuguese Uranium Ores	3/49
MITG-A70	Kaufman, Castillo, Koskela	New Fluorimeters for the Deter- mination of Uranium, MIT Models I, II, III, & IV	7/50 🗸
MITG-A71	Haney	Development of Counting-Rate Meters for Continuous Radio- assay	4/50
MITG-A72	Abrams, Kaufman, Dasher	Extraction of Uranium from Rand Precipitates with Carbon- ates, Part I	6/49
MITG-A73	Barnard, Brunner	Carbonate Extraction of Uranium from Dissolved Low-Grade Hydroxide Precipitates	4/50
MITG-A74	Brunner	Further Studies on the Double Precipitation Process	8 /49
MITG-A75	Barnard	Neutralization of Reduced Rand Leach Solutions	12/49
MITG-A76	Brunner, Barnard, Bailey	Acid Leaching of Low-Grade Uranium Precipitates from Rand Ores	10/49
MITG-A77	Bailey	Retreatment of Low-Grade Hydrox- ide Precipitates by the Phosphate Process	3/50
MITG-A78	Brunner	Acid Digestion-Peroxide Retreat- ment Process	1/50
MITG-179	Galvanek, Kaufman	Application of the Solvent Leach- ing Process for the Concentration of Uranium from Rand Ores	11/49 • "

Number	Authors	Title	Date of Issue
MITG-A80	Schiff	Corrosion Tests in Sulfuric Acid-Ferric Sulfate Leaching of Siliceous Ores	10/49
MITG-A81	Abrams, Kaufman	Extraction of Uranium from Rand Precipitates with Carbon- ates, Part II	2/50
MITG-A82	Pannell	Accuracy of Radioassays Obtain- ed with Improved Automatic Sample Changer	7/49
MITG-A83	Dasher, Macdonald, Oberg	Recovery of Uranium from Rand Gold Ores	1/50
MITG-A84	Kennedy	Use of the Paper Column Separa- tion in Estimation of Microgram Quantities of Uranium	6/50
MITG-A85	Bailey	The Selective Precipitation of Uranium from Reduced Rand Ore Leach Solutions with Tetra- sodium Pyrophosphate	3/50
MITG-A86	Kaufman, Abrams	Extraction of Uranium from Rand Precipitates with Car- bonates, Part III. Tests on Precipitates from Type Y & Z Leach Liquors	7/50
MITG-A87	Oberg	Single Leaching, Part I	10/49
MITG-A88	George	Production of Concentrated Leach Solution	10/49
MITG-A89	Abrams, Kaufman	Effect of Variables in Precipita tion and Non-cyclic Leaching of Rand Ores on Recovery of Uranium and the Grade of Uranium-Bearing Precipitates	n- 6/50 1 3

Number	Authors	Title	Issue
MITG-A90	Bailey	Pseudocementation Inter- ference with Pyrophosphate Precipitation of Single Leach Process X Liquors	7/50
MITG-A91	Abrams	Single-Stage Leach III	7/50
MITG-A92	Brunner	Single-Stage Leaching of Some Rand Ores with Reagents Produced by the SO2-Air Process	7/50
MITG-A93	Schiff	Removal of U from Rand Leach Liquors with Anion-Exchange Resins	7/50
MITG-A94	Haney	Preliminary Experiments on Continuous Radioassay of Radioactive Ores and Mill Products	6/50
MITG-A95	Freyberger	Electrolytic Reduction of Uranyl and Ferric Sulfate Solutions	5/50
MITG-A96	Bailey	Removal of Uranium from Rand Leach Liquors with Anion-Ex- change Resins II. Tests with Process X Leach Liquors	7/50
MITG-A97	Barnard	A Preliminary Study of the Ad- sorption of Uranium (VI) and Other Metallic Ions by Anion- Exchange Resins	8/ 50
MITG-A98	Dasher, Brunner, Abrams	Assaying and Testing of Pre- cipitates from the GML Pilot Plant	5/50
MITG-A99	Pannell, Brunner	Tracer Studies of the Pyro- phosphate Processes	9/50

1

			Date of
<u>Number</u>	Authors	Title	Issue
MITG-A100	Macdonald, Brunner, Dasher, Kaufman	Recovery of Uranium from Rand Gold Ores	8 /50
MITG-A103	Brunner	Simultaneous Precipitation of Uranium and Copper	10/50
MITG-A104	Brunner	Filtration of Leach Residue in Extraction of Uranium from Rand Cyanide Residues	9/50
MITG-A112	Pannell, Haney	Comparison of a High Pressure Ion Chamber and GM Tubes for Continuous Radioassaying in an Ore Plant	2/51
MITG-A113	Rubino	Alpha Counting for Assay of Effluents from a Resin Column Treatment of Uranium Ore Leach Solutions	2/51
MITG-201	George	Magnetic Separation and Miner- alogy of Black Sand Concentrates from California, Idaho, and Mon Gold Placers	1/49 s tana
MITG-B2	Brunner, George	Reserves and Potential Produc- tion of Thorium and Uranium from California Gold Placers	8/48
MITG-B3	George	The Mineralogy and Distribution of Radioactivity in Australian Zircon	5/48
MITG-204	George	Mineralogy, Magnetic Fractiona- tion and Leaching of Heavy- Mineral Concentrates from Climax Molybdenum Corporation	10/48
MITG-205	Dickson, Kaufman	Determination of Thorium in Low-Grade Ores	3/50

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Number	Authors	Title	Date of Issue
MITG-206	Frohling	Concentration and Sizing Tests with the Dutch State Cone	.12/48
MITG-207	Schiff	Acid-Leaching of Western Carnotite Ores	9/48
MITG-208	Pannell, Patrick, Rubino	Self-Absorption of Beta Radia- tion for the Discrimination Between Thorium and Uranium	1/49
MITG-209	M.I.T. Min. Eng. Lab. Staff	By-Product Uranium from Phos- phate Outline of a Research Program	12/48
MITG-210	Gaudin	Preliminary Economic Considera- tions Regarding the Extraction of Uranium from Western Phosphat Rock	11/48 e
MITG-211	Frohling, Dasher, Kaufman	Preliminary Experiments on Pre- cipitation of Uranium from Wet- Process Phosphoric Acid	12/48
MITG-212	Brown	Attrition Scrubbing of Western Carnotite and Roscoelite Ores	3/49
MITG-213	Dasher	Final Report on Carnotite Program	3/49
MITG-214	Pannell, Freyberger	Preliminary Experiments on the Gamma, N Reaction for Analyz- ing and Picking Beryl	3/49
MITG_215	Clevenger	Electrolysis of Uranium-Contain- ing Phosphoric Acid Solutions	4/50
MITG-216	Clevenger	The Effect of Impurities on the Precipitation of Uranium from Phosphoric Acid Solutions with Ammonia, Part I	3/50

Number	Authors	Title	Date of Issue
MITG-217	Clevenger	Precipitation of Uranium from Commercial Phosphoric Acid Solutions	7/49
MITG-218	Woody, Clevenger	Precipitation of Uranium from Anaconda 27 ⁰ Be Phosphoric Acid with Potassium or Calcium Hydroxides	3/50
MITG-219	Roethlisberger	The Use of High Efficiency Gamma Counting for Discrimi- nation Between Thorium and Uranium	8/ 49
MITG-220	Rubino	Radioassay of Products from Precipitated Phosphatic Materi- al	9/49
MITG-221	Clevenger	Continuous Precipitation of Uranium in Commercial Phos- phoric Acid Solutions	1/50
MITG-222	Brown	Wet Scrubbing of Western Phosphate Ores	10/49
MITG-223	Woody	Enriching NH3 Precipitate from Reduced Phosphoric Acid	7/50
MITG-224	Pannell	The Beryl Picker	9/49
MITG-225	Galvanek, Kaufman	Further Studies on Solvent Leaching-U Recovery from Eldorado Concentrate, Congo Precipitate, Rand Precipitate, and Carnotites	3/50
MITG-226	Schiff	Experiments on Anaconda Phos- phoric Acid with Ion-Exchange Resins	7/50
MITG-227	Pannell	Quantitative Determination of Beryllium by Use of the Photo- disintegration Reaction	9/50

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MIT REPORTS (Continued)

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Number	AUGIOIS		TRANC
MITG-228	George	Miscellaneous Precipitants for Uranium in Phosphoric Acid Solutions	3/50
MITG-229	Clevenger	Preliminary Experiments on Leaching Low-Uranium Pre- cipitates from Ammoniated Phosphoric Acid	5/50
MITG-230	George, Woody	Preliminary Mineral Eng. Study of Uranium-Bearing Ore from the Sunshine Mine, Idaho	3/50
MITG-231	George	Recovery of Uranium from Climax Brannerite Concentrate, C-7	3/50
MITG-232	Galvanek	Application of the Solvent Leaching Process for the Con- centration of Uranium from Sunshine Ores	3/50
MITG-233	Barnard	Leaching of Superphosphates with Saturated Solutions	7/50
MITG-234	Brown	Dry Scrubbing of Western Phos- phate Ores	5/50
MITG-235	Dasher, Clevenger, Schiff	Removal of Uranium from Phos- phoric Acid with Monazite	7/50
MITG-236	Freyberger	Alpha Counting for Assay of Ether Leach Solutions	6/50
MITG-237	Haney, Rubino	Further STudy of Simultaneous Radiometric Assay for Thorium and Uranium	10/50
MITG-238	Clevenger	Recovery of Uranium and Vana- dium from Ammonia Process Precipitates	7/50

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Number	Authors	Title	Date of Issue
MITG-239	Kennedy	Purification of Wet-Process Phosphoric Acid by Ether	7/50
MITG-240	Woody, George	Mineral Engineering Studies of Uranium Ore Samples from Sunshine Mine, Kellogg, Idaho	8 /50
MITG-241	Clevenger	Precipitation of Uranium from Florida Phosphoric Acid	6/50
MITG-242	~George	Extraction of Uranium from Florida Leach Zone, Sample E39	6/50
MITG-243	-	See Appendix A-3	-
MITG-244	Ward	A Search for Selective Solvents of Uranium Nitrate from Other Nitrates	1/51
MITG-245	Pannell, Rubino	Some Properties of Uranous Phosphates	9/50
MITG-246	Galvanek	Lyometallurgy of Sulfated Materials	2/51
MITG-247	Bloecher	Lyometallurgy Survey	1/51
MITG-250	Clevenger, Dasher	Recovery of Uranium from Phosphatic Materials	9/50
MITG-251	Grandfield	Fluorimetric Determination of Uranium Part II, A Rapid Metho for the Purification of Uraniu in Solutions where impurity to Uranium Ratio is High	11/50 1 n
MITG-252	Bloecher	Lyometallurgical Tests on Marysvale Uranium Ores	11/50
MITG-254	-	See Appendix A-3	

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Number	Authors	Title	Date of Issue
MITG-255	Woody, Haney	Continuous Radioassay of Carnotite Ore at Monti- cello	12/50
MITG-256	Dasher	Ion Exchange on Solutions	-
MITG-257	Gaudin, Oberg, Kunin	Ion Exchange, Resin in Pulp	-
MITG-259	Pannell, Morrison	A Circuit for the Automatic Control of Counting Rate Meters	12/50
MITG-260	-	See Appendix A-3	-
MITG-261	Pannell	Air Oxidation of Uranous Solutions	12/50
MITG-263	George, Abrams, Galvanek, Bloecher	Preliminary Mineral Engineer- ing Studies of Cupriferous Uranium Ores Rl and R2	1/51
MITG-A66	Kaufman	Miscellaneous Analytical Methods (Paper Strip - Thyocyanate, etc.)	7/54
MITG-101	Oberg, Macdonald	Resin in Pulp Tests	11/51
MITG-A102	Schiff	Ion Exchange on X and Y Solutions	2/51
MITG-A105	Schiff	Ion Exchange on X Solu- tions Using Thickeners	2/51
MITG-A106	Clevenger	Electrolytic Deposition of Uranium from Synthetic Rand Solutions	2/51

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Number	Authors	Title	Date of Issue
MITG-A107	Schiff	Effect of Some Variables on Ion Exchange of Rand Solutions	3/51
MITG-A108	Lower	Synthetic Ion-Exchange Studies	2/51
MITG-A109	Grandfield	Analytical Use of Ferron	_ 6/53
MITG-A110	Woody, Grandfield	Oxidizing Carbonate Leach	2/51
MITG-Alll	Oberg, Macdonald	Resin Life Tester	7/54
MITG-248	Owens	Miscellaneous Potentio- metric Studies of Uranium Solutions	2/51
MITG-253	Brown, George, Kennedy	Mineral Engineering Report on Marysvale Ores Ql, 2, and 3	2/51
MITG-258	Woody, George, Abrams	Recovery of Uranium and By- Product Silver from Uranium Ore Samples - Sunshine Mine, Kellogg, Idaho	2/51
MITG-262	Kennedy, George, Brown,. Bailey, Galvanek, Bloecher	Mineral Engineering Report on Marysvale Ores Q4, 5, 6, and 7	2/51
MITG-264	Bailey, Clevenger, Brunner, Woody, Galvanek, Bloecher, George, Abrams	Utah Cupriferous Uranium Ores	2/51 • *

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<u>MIT_REPORTS</u> (Continued)

Number	Authors	Title	Date of Issue
MITG-265	Bloecher	Economics of Lyometallurgy	2/51
MITG-266	Haney, Dasher	Ether Alarm	2/51